

International Standard



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Laboratory sintered (fritted) filters — Porosity grading, classification and designation

Filtres frittés de laboratoire — Échelle de porosité — Classification et désignation

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Foreword

ISO (the International Organization for Standardization) is a worldwide federation of national standards institutes (ISO member bodies). The work of developing International Standards is carried out through ISO technical committees. Every member body interested in a subject for which a technical committee has been set up has the right to be represented on that committee. International organizations, governmental and non-governmental, in liaison with ISO, also take part in the work.

Draft International Standards adopted by the technical committees are circulated to the member bodies for approval before their acceptance as International Standards by the ISO Council.

International Standard ISO 4793 was developed by Technical Committee ISO/TC 48, *Laboratory glassware and related apparatus*, and was circulated to the member bodies in March 1979.

It has been approved by the member bodies of the following countries :

Australia	Israel	South Africa, Rep. of
Canada	Italy	Spain
Czechoslovakia	Libyan Arab Jamahiriya	Turkey
France	Mexico	United Kingdom
Germany, F. R.	Netherlands	USSR
Hungary	Poland	
India	Romania	

No member body expressed disapproval of the document.

Laboratory sintered (fritted) filters — Porosity grading, classification and designation

1 Scope and field of application

This International Standard specifies a system of porosity grading, classifying and designating laboratory sintered (fritted) filters by the determination of pore size index.

It is applicable to laboratory filters made of glass, vitreous silica, ceramics, metals and plastic materials.

Test methods are included in annexes B and C for the determination of air permeability and uniformity of pore size, but these characteristics do not form part of the requirements of this International Standard.

2 Definitions

2.1 sintered (fritted) filter : A filter produced from porous material formed by the thermal bonding of particles.

2.2 pore size index : A characteristic of a filter related to pore diameter.

2.3 permeability : A characteristic of a filter related to the rate of flow through it under specified conditions.

3 Quality

Filters shall not shed particles under conditions of normal use and shall withstand a working pressure differential of 1,013 bar applied in the normal direction of use.

When tested for pore size index by the method specified in annex A, there shall be no evidence of faults in the filter material, or the sealing into the holder.

4 Grading of filters

Filters shall be graded according to their pore size index in one of the eight grades specified in table 1.

The designation allotted to each grade consists of the upper limit of its pore size index range, expressed in micrometres preceded by the letter "P".

Filters may be provided in certain materials or for special purposes with pore size indexes falling within narrower ranges than those given in table 1; if so, this should be indicated by stating both the minimum and maximum limits of the range.

Table 1 — Grading of filters

Designation of grade	Pore size index, μm	
	$>$	\leq
P 1,6	—	1,6
P 4	1,6	4
P 10	4	10
P 16	10	16
P 40	16	40
P 100	40	100
P 160	100	160
P 250	160	250

5 Limits for pore size index

When the filter is tested in accordance with the method specified in annex A, the pore size index shall be within the limits specified in table 1 for its grade.

NOTE — It is recommended that filters be manufactured with pore size indexes near the centre of the range of the appropriate grade.

6 Uniformity test

If it is required to assess the uniformity of the filter over its working area, the method of test described in annex B should be used.

7 Permeability

If it is required to measure the permeability of the filter, it should be tested in accordance with the method described in annex C, and should not have a permeability less than the value specified in table 2 for its grade.

Table 2 — Permeability of filters

NOTE — The figures given relate to filter discs up to 6 mm thick.

Designation of grade	Minimum permeability (airflow at 1 mbar)	
	m ³ /m ² ·ks	cm ³ /cm ² ·min
P 1,6	0,12	0,72
P 4	0,33	1,98
P 10	0,83	4,98
P 16	1,7	10,2
P 40	5,0	30
P 100	33	198
P 160	67	402
P 250	83	498

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Annex A

Method for determination of pore size index

A.0 This method of test measures the pressure at which the first air bubble breaks away from the filter under specified conditions. This pressure is then used to calculate the equivalent capillary diameter. Thus, the test does not constitute a measurement of pore size but provides an indication of pore diameter, which is related to the maximum size of particle that the filter will pass.

The retentivity of a filter is also affected by other factors.

A.1 Ensure that the filter is thoroughly clean, especially that it is free from detergents, and wettable by the test liquid.

Table 3 lists some of the test liquids that have been found suitable for various filter materials, and that have the desirable properties of low or zero flammability and low toxicity.

In the case of filters made of materials such as glass, vitreous silica, ceramics, platinum, bronze or stainless steel, the choice of the test liquid is wide, in relation to both wettability and non-

reactivity with the filter material. In the case of plastic materials, reactivity is an important consideration, and certain liquids may cause partial dissolution or swelling.

In order to give an adequate reading on a mercury manometer, it is generally preferable to use water as the test liquid on the coarse filters. There may, however, be important reasons for using one of the liquids of low surface tension on some filters, and in such cases it is more appropriate to employ a water manometer and make the necessary correction. Examples are

- 1) polytetrafluoroethylene filters, which are not wetted by water;
- 2) domed filters, for which excessive pressure on the concave side could cause fracture;
- 3) fine grade filters, because the pressure necessary when using water may be greater than that the filter can withstand.

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 Table 3 – Suitable test liquids

Test liquid	Nominal surface tension at 20 °C		Filter material
	N/m	dyn/cm	
Ethanol, 95 % (V/V)	0,022	22	All
Propan-2-ol (iso-propanol)	0,022	22	All
1,1,1-trichloroethane	0,025	25	All except plastic materials
Water	0,073	73	See A.1

NOTE — The surface tension values quoted are sufficiently accurate for the purposes of the test, but they are liable to be affected by contamination of the test liquid (for example by the air supply) and this should be avoided.

A.2 Assemble the filters in a suitable apparatus, for example that illustrated in figure 1.

NOTE — If the filters comprise a fine grade material supported on a coarser grade, the filter characteristics stated should be those of the finer grade and the filter should be tested in such a way that the bubbles appear at the surface of the finer grade material.

Connect an adequate source of clean, dry air, that is supplied at an accurately and finely controlled pressure, for example using a needle valve (the equations in A.5 are based on the assumption of static conditions in the system). Situate the manometer so as to indicate the actual pressure at the filter.

A.3 Cover the filter with a layer of the test liquid, as shallow as is convenient, and ensure that all the pores are impregnated.

Assuming the usual flat form of filter is used, there should be no excessive variation of hydrostatic head over its working area. If this hydrostatic head is significant, convert its value to the appropriate pressure units, and deduct this pressure from the manometer reading to give the effective pressure.

When a domed filter is being tested, bubbles tend to appear first at the uppermost region of the dome, owing to the varying hydrostatic head. It may be desirable in this case to tilt the filter to bring different regions into the uppermost position, to ascertain

- a) the point of maximum pore size index;
- b) the general uniformity of the filter (see annex B).

Hollow filters (for example cylindrical) should be supported with the axis horizontal and suitably rotated.

A.4 Gradually increase the air pressure until the first air bubble breaks away from the surface of the filter. (For hollow filters it is necessary to allow sufficient time to ensure that all free liquid is driven out of the central cavity of the filter.) Read the pressure at the filter from the manometer.

Repeat the test, taking the precautions stated above, with the pressure being increased more slowly. If concordant results are obtained the test has been performed satisfactorily.

A.5 Calculate the pore size index, d , in micrometres (μm), using either of the following formulae

$$\text{a) } \frac{40 \gamma_1}{P_1}$$

where

γ_1 is the surface tension, in newtons per metre, of the test liquid;

P_1 is the effective pressure, in bars;

$$\text{b) } \frac{30 \gamma_2}{P_2}$$

where

γ_2 is the surface tension, in dynes per centimetre, of the test liquid;

P_2 is the effective pressure, in millimetres of mercury.

NOTES

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$$1 \text{ bar} = 10^5 \text{ N/m}^2 = 750,24 \text{ mm Hg}$$

2 If a manometer liquid other than mercury is used, the actual reading of the manometer should be converted to bars or millimetres of mercury, as required.

3 The manometer may be calibrated or a graph constructed for a particular test liquid, so that the pore size index can be read directly.

A.6 When the pore size index has been determined, the filter may be left connected to the apparatus and its uniformity checked as described in annex B.

Annex B

Procedure for assessing uniformity of filters

B.1 Use the procedure specified in annex A for determination of pore size index.

B.2 Following the appearance of the first air bubble, as

described in A.4, increase the air pressure until bubbles emerge uniformly over the upper surface and note the new pressure readings. This should correspond to a pore size index not less than the minimum for the grade (see table 1).

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Annex C

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Method for determination of air permeability

C.0 This method measures the rate of flow of air through a filter under specified conditions. It is related (but not necessarily by simple proportionality) to the rate of liquid flow through the filter, and hence to the speed of filtration.

C.1 Ensure that the filter is thoroughly clean and dry.

Assemble the filter in a suitable apparatus, for example that illustrated in figure 2. Establish a suitable pressure difference P_3 (for example 1 mbar) across the filter and maintain this during the test. Measure the air flow rate Q by means of a suitable air flow meter, and convert the rate to cubic metres per kilosecond or cubic centimetres per minute, as required.

C.2 Determine the effective surface area A of the filter in square metres or square centimetres, as required, making

allowance for the part of the filter near the edge which is rendered ineffective by the fixing process.

C.3 Calculate the air permeability per millibar pressure difference, expressed in cubic metres per square metre kilosecond [$\text{m}^3/(\text{m}^2 \cdot \text{ks})$] or cubic centimetres per square centimetre minute [$\text{cm}^3/(\text{cm}^2 \cdot \text{min})$], as required, from the formula

$$\frac{Q}{A P_3}$$

NOTE — The test assumes viscous flow of air through the filter, and is adequate for the general requirements of laboratory sintered filters. For particular purposes, for example filters required for accurate work in fluid flow, more detailed tests may be required and should be agreed upon by the interested parties.

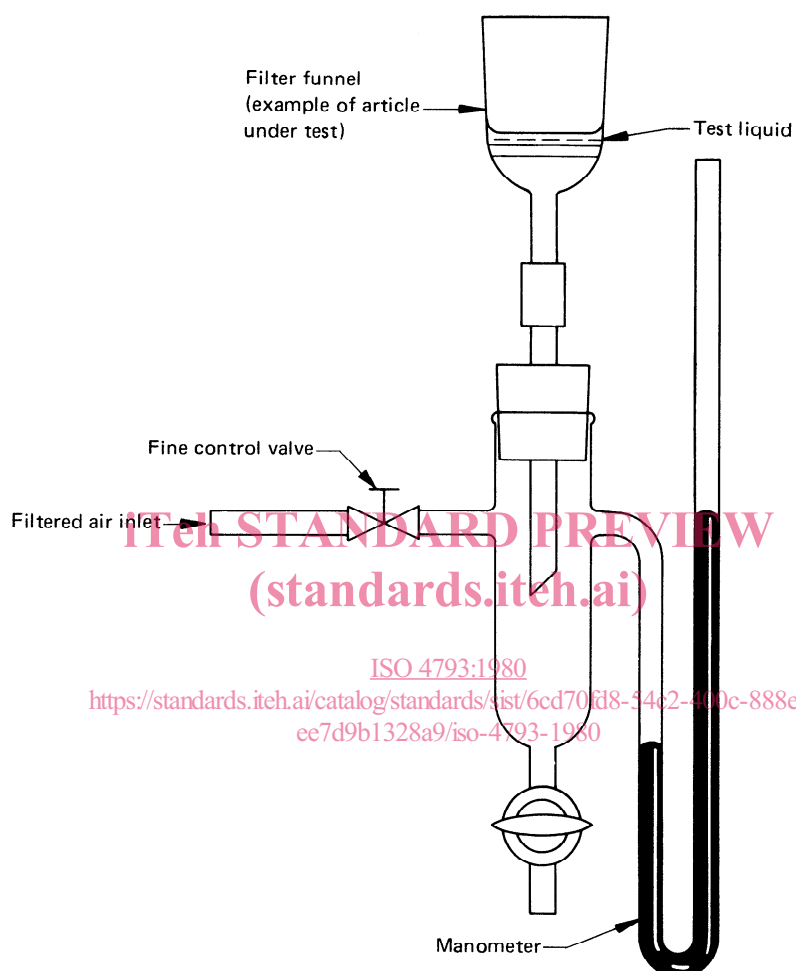


Figure 1 — Apparatus for determination of pore size index

WARNING — For safety reasons, this apparatus must be suitably shielded when in use.

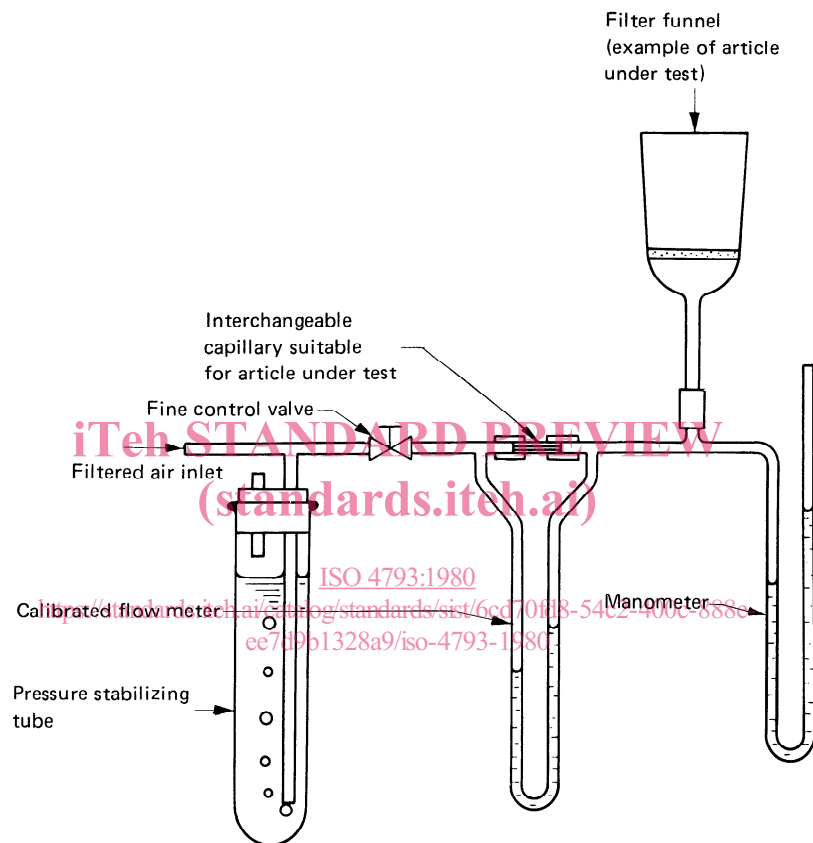


Figure 2 — Apparatus for determination of air permeability