# Standard Test Method for Calculation of Volume and Weight of Industrial Aromatic Hydrocarbons and Cyclohexane ${ }^{1}$ 


#### Abstract

This standard is issued under the fixed designation D1555; the number immediately following the designation indicates the year of original adoption or, in the case of revision, the year of last revision. A number in parentheses indicates the year of last reapproval. A superscript epsilon ( $\varepsilon$ ) indicates an editorial change since the last revision or reapproval.


This standard has been approved for use by agencies of the U.S. Department of Defense.

## 1. Scope

1.1 This standard is for use in calculating the weight and volume of benzene, toluene, mixed xylenes, styrene, orthoxylene, meta-xylene, para-xylene, cumene, ethylbenzene, 300 to $350^{\circ} \mathrm{F}$ and 350 to $400^{\circ} \mathrm{F}$ aromatic hydrocarbons, and cyclohexane. A method is given for calculating the volume at a desired temperature $t_{b}{ }^{\circ} \mathrm{F}$ from an observed volume at $t_{o}{ }^{\circ} \mathrm{F}$. Table 1 lists the density in Vacuo at $60^{\circ} \mathrm{F}$ for chemicals used to develop the relationship. Densities (or weights) "in vacuo" represent the true density (or weight) if measured in a vacuum without the buoyancy effect of air acting on the liquid. It is representative of the actual amount of product present. Densities (or weights) "in air" represent what would actually be measured on a scale. The difference is on the order of $0.13 \%$. Modern densitometers measure density in vacuo and the ASTM recommends the use of in vacuo densities (or weights).
1.2 The values stated in inch-pound units are to be regarded as standard. No other units of measurement are included in this standard.
1.2.1 A complete SI unit companion standard has been developed in Test Method D1555M.
1.3 This standard does not purport to address all of the safety concerns, if any, associated with its use. It is the responsibility of the user of this standard to establish appropriate safety, health, and environmental practices and determine the applicability of regulatory limitations prior to use.
1.4 This international standard was developed in accordance with internationally recognized principles on standardization established in the Decision on Principles for the Development of International Standards, Guides and Recommendations issued by the World Trade Organization Technical Barriers to Trade (TBT) Committee.

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## 2. Referenced Documents

2.1 ASTM Standards: ${ }^{2}$

D1217 Test Method for Density and Relative Density (Specific Gravity) of Liquids by Bingham Pycnometer
D1555M Test Method for Calculation of Volume and Weight of Industrial Aromatic Hydrocarbons and Cyclohexane [Metric]
D3505 Test Method for Density or Relative Density of Pure Liquid Chemicals
D4052 Test Method for Density, Relative Density, and API Gravity of Liquids by Digital Density Meter

### 2.2 Other Documents:

American Petroleum Society Research Project $44^{3}$
Patterson, J. B., and Morris, E. C. Metrologia, 31, 1994, pp. 277-288
NSRDS-NIST 75-121 TRC Thermodynamic TablesHydrocarbons, Supplement No. 121, April 30, $2001^{4}$

## 3. Significance and Use

3.1 This test method is suitable for use in calculating weights and volumes of the products outlined in Section 1. The information presented in this method can be used for determining quantities of the above-stated aromatic hydrocarbons in tanks, shipping containers, etc.

## 4. Basic Data

4.1 Densities of materials should be determined by measurement (see Section 7). Densities of pure materials at $60^{\circ} \mathrm{F}$ may be estimated from densities furnished by NSRDS-NIST 75-121 (National Standard Reference Data Series-National Institute of Standards and Technology).

[^1]TABLE 1 Physical Properties
\(\left.\left.$$
\begin{array}{lcccc}\hline \text { Product } & \begin{array}{c}\text { Freezing } \\
\text { Point } \\
{ }^{\circ} \mathrm{F}\end{array} & 42.0 & \begin{array}{c}\text { Boiling } \\
\text { Point } \\
{ }^{\circ} \mathrm{F}\end{array} & \begin{array}{c}\text { Density } \\
\text { in Vacuo } \\
\text { at } 60^{\circ} \mathrm{F} \mathrm{g} / \mathrm{cc}^{\mathrm{A}, B}\end{array}\end{array}
$$ $$
\begin{array}{c}\text { Density in Vacuo } \\
\text { at } 60^{\circ} \mathrm{F} \\
\mathrm{lb} / \mathrm{gal}^{\mathrm{C}}\end{array}
$$\right] \begin{array}{c}Density in Air <br>
at 60^{\circ} \mathrm{F} <br>

\mathrm{lb} / \mathrm{gal}^{D}\end{array}\right]\)| 7.3662 |
| :--- |
| Benzene |

${ }^{\text {A }}$ Based on regression of 2001 TRC Thermodynamic Tables, Hydrocarbons, NSRDS-NIST 75-121 (April 30, 2001). The data is presented in Appendix X1.
${ }^{B}$ Specific Gravity has been deleted from this table as unnecessary to this standard. If needed, divide $60^{\circ} \mathrm{F}$ density in g/cc by $0.999016 \mathrm{~g} / \mathrm{cc}$. See Appendix X2.
${ }^{c}$ Produced by multiplying the density in vacuo at $60^{\circ} \mathrm{F}$ in $\mathrm{g} / \mathrm{cc}$ by 8.345404452 and rounding to 4 decimal places.
${ }^{D}$ Produced using Density - g/cc in air $\left.\cdot 1.000149926-0.001199407795\right) \cdot 8.345404452$, rounding to 4 decimal places. See Appendix X3.
4.2 The VCF (Volume Correction Factor) equations provided below were derived from the Volume Correction Tables presented in the previous edition of this standard, Method D1555-95. Although reported as based on the American Petroleum Institute Research Project 44, the actual documentation that could be found is incomplete. As regression of the NIST data (Appendix X1) provided VCFs that differ from the historical VCFs by only 0 to $\pm 0.12 \%$ (depending on the compound), a decision was made to use the previous method's VCF tables.
4.3 The VCF tables were regressed with a commercially available data regression program (TableCurve 2D V4). However, any modern regression program should produce the same results.
4.4 The former VCF tables were based on data for compounds used in American Petroleum Institute Research Project 44 for which the purity is not clearly defined, but were reported to be usable for materials in the ranges indicated in Table 2. The data supporting this conclusion appears to be unavailable at the present time; however there is no reason to change this recommendation. If, depending on the composition of the impurities, there is reason to suspect that the VCF implementation procedures presented below do not apply to a particular impure product, a separate implementation procedure should be independently determined. This may be done by measuring the density of a representative sample at different temperatures throughout the expected working temperature range, regressing the data to obtain a temperature/density equation that best

TABLE 2 Application Range of Implementation Procedure

| Impure Products | Range |
| :--- | :--- |
| Benzene | 95 to $100 \%$ |
| Cumene | 95 to $100 \%$ |
| Cyclohexane | 90 to $100 \%$ |
| Ethylbenzene | 95 to $100 \%$ |
| Styrene | 95 to $100 \%$ |
| Toluene | 95 to $100 \%$ |
| Mixed Xylenes | All proportions |
| $m$-Xylene | 95 to $100 \%$ |
| $0-$ Xylene | 95 to $100 \%$ |
| $p-$ Xylene | 94 to $100 \%$ |
| $300-350^{\circ}$ F Aromatic Hydrocarbons | All proportions |
| $350-400^{\circ}$ F Aromatic Hydrocarbons | All proportions |

reproduces the observed data, and then dividing the constants of the temperature/density equation by the calculated density at $60^{\circ} \mathrm{F}$.

## 5. Volume Correction Factor Implementation Procedure

5.1 The following general equation is used to generate the Volume Correction Factors:

$$
\begin{equation*}
V C F=\frac{a+b t_{o}+c t_{o}^{2}+d t_{o}^{3}+e t_{o}^{4}}{a+b t_{b}+c t_{b}^{2}+d t_{b}^{3}+e t_{b}^{4}} \tag{1}
\end{equation*}
$$

where:
$t_{o}=$ observed temperature, and
$t_{b}=$ base temperature where value is needed.
and constants a through e are specific to each compound (presented in Table 3).
5.1.1 Temperature may be entered in tenths of a degree Fahrenheit.
5.1.2 The calculated result is rounded to the appropriate significant figures if it is to be reported and not rounded if to be used in another calculation. No intermediate rounding or truncation should be done.
5.1.3 The equations are valid for liquid product up to $140^{\circ} \mathrm{F}$ ( $150^{\circ} \mathrm{F}$ for $p$-xylene).
5.1.4 This implementation procedure replaces the printed table in a previous edition of this standard (Method D1555-95) for determining VCFs. The implementation procedure is the Standard, not the printed table. However, the printed table is provided in $1^{\circ} \mathrm{F}$ increments for the user's convenience (Table 4).

## 6. Use of the Implementation Procedure

6.1 Convert Volume to $60^{\circ} \mathrm{F}$-Enter the appropriate equation with the temperature to the nearest 0.1 degree Fahrenheit at which the bulk volume was measured (temperature $t$ ). Multiply the bulk volume measurement at temperature $t$ by the VCF.
6.1.1 Example 1 -What is the volume at $60^{\circ} \mathrm{F}$ of a tank car of $p$-xylene whose volume was measured to be 9280 gal at a mean temperature of $88.7^{\circ} \mathrm{F}$ ?

TABLE 3 VCF Constants

| Product | a | b | c | d |
| :--- | :---: | :---: | :---: | :---: |
| Benzene | 1.038382492 | $-6.2307 \times 10^{-4}$ | $-2.8505 \times 10^{-7}$ | 0 |
| Cumene | 1.032401114 | $-5.3445 \times 10^{-4}$ | $-9.5067 \times 10^{-8}$ | $1.2692 \times 10^{-10}$ |
| Cyclohexane | 1.039337296 | $-6.4728 \times 10^{-4}$ | $-1.4582 \times 10^{-7}$ | $3.6272 \times 10^{-11}$ |
| Ethylbenzene | 1.033346632 | $-5.5243 \times 10^{-4}$ | $8.37035 \times 10^{-10}$ | $1.03538 \times 10^{-10}$ |
| Styrene | 1.032227515 | $-5.3444 \times 10^{-4}$ | $-4.4323 \times 10^{-8}$ | $-1.2692 \times 10^{-9}$ |
| Toluene | 1.035323647 | $-5.8887 \times 10^{-4}$ | $2.46508 \times 10^{-9}$ | 0 |
| $m$-Xylene ${ }^{\text {A }}$ | 1.031887514 | $-5.2326 \times 10^{-4}$ | $-1.3253 \times 10^{-7}$ | $-7.2802 \times 10^{-12}$ |
| $o-$ Xylene | 1.031436449 | $-5.2302 \times 10^{-4}$ | $-2.5217 \times 10^{-9}$ | $-7.35960 \times 10^{-11}$ |
| $p-$ Xylene | 1.032307000 | $-5.2815 \times 10^{-4}$ | $-1.8416 \times 10^{-7}$ | $-2.13840 \times 10^{-10}$ |
| $300-350^{\circ} \mathrm{F}$ | 1.031118000 | $-5.1827 \times 10^{-4}$ | $-3.5109 \times 10^{-9}$ | 0 |
| $350-400^{\circ} \mathrm{F}$ | 1.029099000 | $-4.8287 \times 10^{-4}$ | $-3.7692 \times 10^{-8}$ | $-1.89256 \times 10^{-10}$ |

${ }^{A}$ And mixed xylenes.
6.1.1.1 Enter $88.7^{\circ} \mathrm{F}$ and the appropriate constants from Table 3 into Eq 1 to calculate a VCF of 0.984143256178277. Multiply the volume at $88.7^{\circ} \mathrm{F}$ by the VCF to obtain the volume at $60^{\circ} \mathrm{F}$.

```
9280 gal }\times0.984143256178277=9,132.84941733442 or 9133 gal
```

If this value is to be reported, it may be rounded as required by the user. The unrounded intermediate value should be used for additional calculations.
6.2 Converting Volume to Weight for Chemicals Listed in Table 1-Convert the measured bulk volume to gallons at $60^{\circ} \mathrm{F}$ as described in 6.1. Determine the density (all weights in vacuo) at $60^{\circ} \mathrm{F}$ in grams per milliliter (equivalent to grams per cubic centimeter and kilograms per liter) as described in Section 7. To obtain the weight multiply the density in pound per gallon and the volume in gallons. To obtain the density in pounds per gallon in vacuo multiple the measured density by 8.345404452. To obtain the pounds per gallon in air at $60^{\circ} \mathrm{F}$, use the following equation to determine the pound per gallon in air, refer to Appendix X3.

$$
\begin{aligned}
\mathrm{D}_{\text {lb per gallon in air at } 60 \mathrm{~F}}= & {\left[1.000149926 \times \mathrm{D}_{\text {in vacuo at } 60 \mathrm{~F}}\right.} \\
& -0.00119940779543] \times 8.345404452
\end{aligned}
$$

To obtain the weight in pounds, multiply the density in pounds per gallon by the volume in gallons.
6.2.1 The density of the $p$-xylene in Example 1 was determined by Test Method D4052 to be $0.8646 \mathrm{~g} / \mathrm{mL}$ (in vacuo) at $60^{\circ} \mathrm{F}$. The weight is:

$$
\begin{aligned}
& 9280 \mathrm{gal} \times 0.984143256178277 \times 8.345404452 \times 0.8646 \\
& \quad=65.897 .4967627663 \quad \mathrm{lb}_{\text {in vacuo }} \\
& 9280 \mathrm{gal} \times 0.984143256178277 \times 8.345404452 \\
& \quad \times\left[\begin{array}{llll}
1.000149926 & \times 0.8646-0.0011994077951
\end{array}\right] \\
& \quad=65,815.960860521 \quad \mathrm{lb}_{\text {in air }}
\end{aligned}
$$

or

If this value is to be reported, it may be rounded as required by the user. The unrounded intermediate value should be used for additional calculations.

## 7. Density Determination

7.1 Density determinations may be carried out by any procedure known to be reliable to at least 4 digits. Test Methods D1217, D3505, and D4052 are suitable and are written to give density in vacuo. They should be used with caution, however, as they may be using older data than that upon which this standard is based upon.

## 8. Precision and Bias

8.1 Since this is a calculation method, no precision and bias statement is required.

## 9. Keywords

9.1 aromatic; benzene; calculation; conversion; cumene; density; ethylbenzene; in air; in vacuo; m-xylene; mixed xylene; $o$-xylene; $p$-xylene; specific gravity; styrene; 300 to $350^{\circ} \mathrm{F}$ aromatic hydrocarbons; 350 to $400^{\circ} \mathrm{F}$ aromatic hydrocarbons; toluene; volume; weight

TABLE 4 Volume Correction Factors

| Volume Correction to $60^{\circ} \mathrm{F}$ |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Temperature ${ }^{\circ} \mathrm{F}$ | Benzene | Cumene | Cyclohexane | Ethylbenzene | Styrene | Toluene |  | o-Xylene | $p$-Xylene | 300 to $350^{\circ}$ <br> Aromatic Hydrocarbons | 350 to $400^{\circ}$ Aromatic Hydrocarbons |
| -5.0 | ... | ... | ... | ... | ... | 1.03827 | ... | ... | ... | ... | ... |
| -4.0 | ... | ... | ... | ... | ... | 1.03768 | ... | ... | ... | ... | ... |
| -3.0 | ... | ... | ... | ... | ... | 1.03709 | ... | ... | ... | ... | ... |
| -2.0 | ... | ... | ... | ... | ... | 1.03650 | $\ldots$ | ... | ... | ... | ... |
| -1.0 | ... | $\ldots$ | ... | ... | ... | 1.03591 | $\ldots$ | ... | ... | ... | ... |
| 0.0 | ... | $\ldots$ | ... | ... | ... | 1.03532 | ... | ... | ... | ... | ... |
| 1.0 | ... | ... | ... | ... | ... | 1.03473 | ... | ... | ... | ... | ... |
| 2.0 | ... | $\ldots$ | ... | ... | ... | 1.03415 | ... | ... | ... | ... | ... |
| 3.0 | ... | ... | ... | ... | ... | 1.03356 | ... | ... | $\ldots$ | ... | ... |
| 4.0 | ... | ... | ... | ... | ... | 1.03297 | ... | ... | ... |  |  |
| 5.0 | ... | 1.02973 | ... | 1.03058 | ... | 1.03238 | 1.02927 | 1.02882 | ... | 1.02853 | 1.02668 |
| 6.0 | ... | 1.02919 | ... | 1.03003 | ... | 1.03179 | 1.02874 | 1.02830 | ... | 1.02801 | 1.02620 |
| 7.0 | ... | 1.02866 | ... | 1.02948 | ... | 1.03120 | 1.02822 | 1.02778 | ... | 1.02749 | 1.02572 |
| 8.0 | ... | 1.02812 | ... | 1.02893 | ... | 1.03061 | 1.02769 | 1.02725 | ... | 1.02697 | 1.02523 |
| 9.0 | ... | 1.02758 | ... | 1.02837 | ... | 1.03002 | 1.02717 | 1.02673 | ... | 1.02645 | 1.02475 |
| 10.0 | ... | 1.02705 | ... | 1.02782 | ... | 1.02944 | 1.02664 | 1.02621 | ... | 1.02593 | 1.02427 |
| 11.0 | ... | 1.02651 | ... | 1.02727 | ... | 1.02885 | 1.02612 | 1.02568 | ... | 1.02542 | 1.02378 |
| 12.0 | ... | 1.02597 | ... | 1.02672 | ... | 1.02826 | 1.02559 | 1.02516 | ... | 1.02490 | 1.02330 |
| 13.0 | ... | 1.02544 | ... | 1.02616 | ... | 1.02767 | 1.02506 | 1.02464 | ... | 1.02438 | 1.02282 |
| 14.0 | ... | 1.02490 | ... | 1.02561 |  | 1.02708 | 1.02454 | 1.02411 | ... | 1.02386 | 1.02233 |
| 15.0 | ... | 1.02436 | ... | 1.02506 | 1.02420 | 1.02649 | 1.02401 | 1.02359 | ... | 1.02334 | 1.02185 |
| 16.0 | ... | 1.02383 | ... | 1.02450 | 1.02367 | 1.02590 | 1.02348 | 1.02307 | ... | 1.02282 | 1.02136 |
| 17.0 | ... | 1.02329 | ... | 1.02395 | 1.02313 | 1.02531 | 1.02295 | 1.02254 | ... | 1.02231 | 1.02088 |
| 18.0 | ... | 1.02275 | ... | 1.02340 | 1.02259 | 1.02472 | 1.02243 | 1.02202 | ... | 1.02179 | 1.02040 |
| 19.0 | ... | 1.02221 | ... | 1.02284 | 1.02206 | 1.02414 | 1.02190 | 1.02150 | ... | 1.02127 | 1.01991 |
| 20.0 | ... | 1.02167 | $\ldots$ | 1.02229 | 1.02152 | 1.02355 | 1.02137 | 1.02097 | ... | 1.02075 | 1.01943 |
| 21.0 | ... | 1.02114 | ... | 1.02174 | 1.02098 | 1.02296 | 1.02084 | 1.02045 | ... | 1.02023 | 1.01894 |
| 22.0 | ... | 1.02060 | $\ldots$ | 1.02118 | 1.02045 | 1.02237 | 1.02031 | 1.01993 | $\ldots$ | 1.01971 | 1.01846 |
| 23.0 | ... | 1.02006 | ... | 1.02063 | 1.01991 | 1.02178 | 1.01978 | 1.01940 | ... | 1.01920 | 1.01797 |
| 24.0 | $\ldots$ | 1.01952 | $\ldots$ | 1.02007 | 1.01938 | 1.02119 | 1.01925 | 1.01888 | ... | 1.01868 | 1.01749 |
| 25.0 | ... | 1.01898 | ... | 1.01952 | 1.01884 | 1.02060 | 1.01872 | 1.01836 | ... | 1.01816 | 1.01700 |
| 26.0 | ... | 1.01844 | ... | 1.01896 | 1.01830 | 1.02001 | 1.01819 | 1.01783 | ... | 1.01764 | 1.01652 |
| 27.0 | ... | 1.01790 | ... | 1.01841 | 1.01777 | 1.01943 | 1.01766 | 1.01731 | ... | 1.01712 | 1.01603 |
| 28.0 | ... | 1.01736 | ... | 1.01785 | 1.01723 | 1.01884 | 1.01713 | 1.01679 | ... | 1.01660 | 1.01555 |
| 29.0 | ... | 1.01682 | ... | 1.01730 | 1.01669 | 1.01825 | 1.01660 | 1.01626 | ... | 1.01608 | 1.01506 |
| 30.0 | ... | 1.01628 | ... | 1.01674 | 1.01615 | 1.01766 | 1.01607 | 1.01574 | ... | 1.01557 | 1.01458 |
| 31.0 | ... | 1.01574 | ... | 1.01619 | 1.01562 | 1.01707 | 1.01554 | 1.01521 | ... | 1.01505 | 1.01409 |
| 32.0 | ... | 1.01520 | ... | 1.01563 | 1.01508 | 1.01648 | 1.01501 | 1.01469 | ... | 1.01453 | 1.01361 |
| 33.0 | ... | 1.01466 | ... | 1.01508 | 1.01454 | 1.01589 | 1.01447 | 1.01417 | ... | 1.01401 | 1.01312 |
| 34.0 | ... | 1.01412 | \% | 1.01452 | 1.01401 | 1.01530 | 1.01394 | 1.01364 | ... | 1.01349 | 1.01264 |
| 35.0 | ... | 1.01358 | $\ldots$ | 1.01397 | 1.01347 | 1.01472 | 1.01341 | 1.01312 | ... | 1.01297 | 1.01215 |
| 36.0 | ... | 1.01304 | ... | 1.01341 | 1.01293 | 1.01413 | 1.01287 | 1.01259 | ... | 1.01245 | 1.01167 |
| 37.0 | ... | 1.01250 | ... | 1.01285 | 1.01239 | 1.01354 | 1.01234 | 1.01207 | ... | 1.01194 | 1.01118 |
| 38.0 | ... | 1.01196 | ... | 1.01230 | 1.01185 | 1.01295 | 1.01181 | 1.01155 | ... | 1.01142 | 1.01070 |
| 39.0 | ... | 1.01142 | ... | 1.01174 | 1.01132 | 1.01236 | 1.01127 | 1.01102 | ... | 1.01090 | 1.01021 |
| 40.0 | ... | 1.01087 | ... | 1.01118 | 1.01078 | 1.01177 | 1.01074 | 1.01050 | ... | 1.01038 | 1.00973 |
| 41.0 | ... | 1.01033 | ... | 1.01063 | 1.01024 | 1.01118 | 1.01021 | 1.00997 | ... | 1.00986 | 1.00924 |
| 42.0 |  | 1.00979 | ... | 1.01007 | 1.00970 | 1.01059 | 1.00967 | 1.00945 | ... | 1.00934 | 1.00875 |
| 43.0 | 1.01107 | 1.00925 |  | 1.00951 | 1.00916 | 1.01001 | 1.00914 | 1.00892 | ... | 1.00882 | 1.00827 |
| 44.0 | 1.01043 | 1.00870 | 1.01058 | 1.00895 | 1.00863 | 1.00942 | 1.00860 | 1.00840 | ... | 1.00831 | 1.00778 |
| 45.0 | 1.00978 | 1.00816 | 1.00992 | 1.00840 | 1.00809 | 1.00883 | 1.00807 | 1.00788 | ... | 1.00779 | 1.00730 |
| 46.0 | 1.00913 | 1.00762 | 1.00926 | 1.00784 | 1.00755 | 1.00824 | 1.00753 | 1.00735 | ... | 1.00727 | 1.00681 |
| 47.0 | 1.00848 | 1.00708 | 1.00860 | 1.00728 | 1.00701 | 1.00765 | 1.00699 | 1.00683 | ... | 1.00675 | 1.00632 |
| 48.0 | 1.00783 | 1.00653 | 1.00794 | 1.00672 | 1.00647 | 1.00706 | 1.00646 | 1.00630 | ... | 1.00623 | 1.00584 |
| 49.0 | 1.00718 | 1.00599 | 1.00728 | 1.00616 | 1.00593 | 1.00647 | 1.00592 | 1.00578 | ... | 1.00571 | 1.00535 |
| 50.0 | 1.00653 | 1.00545 | 1.00662 | 1.00560 | 1.00539 | 1.00589 | 1.00538 | 1.00525 | ... | 1.00519 | 1.00487 |
| 51.0 | 1.00588 | 1.00490 | 1.00596 | 1.00504 | 1.00486 | 1.00530 | 1.00485 | 1.00473 | ... | 1.00467 | 1.00438 |
| 52.0 | 1.00523 | 1.00436 | 1.00530 | 1.00448 | 1.00432 | 1.00471 | 1.00431 | 1.00420 | ... | 1.00416 | 1.00389 |
| 53.0 | 1.00458 | 1.00381 | 1.00464 | 1.00393 | 1.00378 | 1.00412 | 1.00377 | 1.00368 | ... | 1.00364 | 1.00341 |
| 54.0 | 1.00393 | 1.00327 | 1.00398 | 1.00337 | 1.00324 | 1.00353 | 1.00323 | 1.00315 | ... | 1.00312 | 1.00292 |
| 55.0 | 1.00327 | 1.00272 | 1.00331 | 1.00281 | 1.00270 | 1.00294 | 1.00270 | 1.00263 |  | 1.00260 | 1.00243 |
| 56.0 | 1.00262 | 1.00218 | 1.00265 | 1.00224 | 1.00216 | 1.00235 | 1.00216 | 1.00210 | 1.00219 | 1.00208 | 1.00195 |
| 57.0 | 1.00196 | 1.00164 | 1.00199 | 1.00168 | 1.00162 | 1.00176 | 1.00162 | 1.00158 | 1.00164 | 1.00156 | 1.00146 |
| 58.0 | 1.00131 | 1.00109 | 1.00132 | 1.00112 | 1.00108 | 1.00118 | 1.00108 | 1.00105 | 1.00109 | 1.00104 | 1.00097 |
| 59.0 | 1.00066 | 1.00055 | 1.00066 | 1.00056 | 1.00054 | 1.00059 | 1.00054 | 1.00053 | 1.00054 | 1.00052 | 1.00049 |
| 60.0 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 |
| 61.0 | 0.99934 | 0.99945 | 0.99933 | 0.99944 | 0.99946 | 0.99941 | 0.99946 | 0.99947 | 0.99945 | 0.99949 | 0.99951 |
| 62.0 | 0.99869 | 0.99891 | 0.99867 | 0.99888 | 0.99892 | 0.99882 | 0.99892 | 0.99895 | 0.99890 | 0.99897 | 0.99903 |
| 63.0 | 0.99803 | 0.99836 | 0.99801 | 0.99832 | 0.99838 | 0.99823 | 0.99838 | 0.99842 | 0.99835 | 0.99845 | 0.99854 |
| 64.0 | 0.99737 | 0.99782 | 0.99734 | 0.99775 | 0.99784 | 0.99764 | 0.99784 | 0.99790 | 0.99780 | 0.99793 | 0.99805 |
| 65.0 | 0.99671 | 0.99727 | 0.99668 | 0.99719 | 0.99730 | 0.99706 | 0.99730 | 0.99737 | 0.99725 | 0.99741 | 0.99756 |

TABLE 4 Continued

| Volume Correction to $60^{\circ} \mathrm{F}$ |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Temperature ${ }^{\circ} \mathrm{F}$ | Benzene | Cumene | Cyclohexane | Ethylbenzene | Styrene | Toluene | m-Xylene and Mixed Xylenes | o-Xylene | $p$-Xylene | $\begin{gathered} 300 \text { to } 350^{\circ} \\ \text { Aromatic } \\ \text { Hydrocarbons } \end{gathered}$ | $\begin{gathered} 350 \text { to } 400^{\circ} \\ \text { Aromatic } \\ \text { Hydrocarbons } \end{gathered}$ |
| 66.0 | 0.99605 | 0.99672 | 0.99601 | 0.99663 | 0.99676 | 0.99647 | 0.99675 | 0.99684 | 0.99670 | 0.99689 | 0.99708 |
| 67.0 | 0.99540 | 0.99618 | 0.99535 | 0.99607 | 0.99622 | 0.99588 | 0.99621 | 0.99632 | 0.99615 | 0.99637 | 0.99659 |
| 68.0 | 0.99474 | 0.99563 | 0.99468 | 0.99550 | 0.99568 | 0.99529 | 0.99567 | 0.99579 | 0.99560 | 0.99585 | 0.99610 |
| 69.0 | 0.99408 | 0.99508 | 0.99401 | 0.99494 | 0.99514 | 0.99470 | 0.99513 | 0.99527 | 0.99505 | 0.99533 | 0.99561 |
| 70.0 | 0.99341 | 0.99454 | 0.99335 | 0.99438 | 0.99460 | 0.99411 | 0.99458 | 0.99474 | 0.99450 | 0.99482 | 0.99513 |
| 71.0 | 0.99275 | 0.99399 | 0.99268 | 0.99382 | 0.99406 | 0.99352 | 0.99404 | 0.99421 | 0.99395 | 0.99430 | 0.99464 |
| 72.0 | 0.99209 | 0.99344 | 0.99202 | 0.99325 | 0.99352 | 0.99294 | 0.99350 | 0.99369 | 0.99340 | 0.99378 | 0.99415 |
| 73.0 | 0.99143 | 0.99289 | 0.99135 | 0.99269 | 0.99298 | 0.99235 | 0.99295 | 0.99316 | 0.99284 | 0.99326 | 0.99366 |
| 74.0 | 0.99077 | 0.99235 | 0.99068 | 0.99212 | 0.99244 | 0.99176 | 0.99241 | 0.99263 | 0.99229 | 0.99274 | 0.99318 |
| 75.0 | 0.99010 | 0.99180 | 0.99001 | 0.99156 | 0.99190 | 0.99117 | 0.99187 | 0.99211 | 0.99174 | 0.99222 | 0.99269 |
| 76.0 | 0.98944 | 0.99125 | 0.98935 | 0.99099 | 0.99135 | 0.99058 | 0.99132 | 0.99158 | 0.99119 | 0.99170 | 0.99220 |
| 77.0 | 0.98877 | 0.99070 | 0.98868 | 0.99043 | 0.99081 | 0.98999 | 0.99078 | 0.99105 | 0.99063 | 0.99118 | 0.99171 |
| 78.0 | 0.98811 | 0.99015 | 0.98801 | 0.98987 | 0.99027 | 0.98940 | 0.99023 | 0.99052 | 0.99008 | 0.99066 | 0.99122 |
| 79.0 | 0.98744 | 0.98960 | 0.98734 | 0.98930 | 0.98973 | 0.98881 | 0.98969 | 0.99000 | 0.98953 | 0.99014 | 0.99074 |
| 80.0 | 0.98678 | 0.98906 | 0.98667 | 0.98874 | 0.98919 | 0.98823 | 0.98914 | 0.98947 | 0.98897 | 0.98962 | 0.99025 |
| 81.0 | 0.98611 | 0.98851 | 0.98601 | 0.98817 | 0.98865 | 0.98764 | 0.98859 | 0.98894 | 0.98842 | 0.98910 | 0.98976 |
| 82.0 | 0.98544 | 0.98796 | 0.98534 | 0.98760 | 0.98811 | 0.98705 | 0.98805 | 0.98841 | 0.98786 | 0.98859 | 0.98927 |
| 83.0 | 0.98478 | 0.98741 | 0.98467 | 0.98704 | 0.98756 | 0.98646 | 0.98750 | 0.98789 | 0.98731 | 0.98807 | 0.98878 |
| 84.0 | 0.98411 | 0.98686 | 0.98400 | 0.98647 | 0.98702 | 0.98587 | 0.98695 | 0.98736 | 0.98676 | 0.98755 | 0.98829 |
| 85.0 | 0.98344 | 0.98631 | 0.98333 | 0.98591 | 0.98648 | 0.98528 | 0.98641 | 0.98683 | 0.98620 | 0.98703 | 0.98781 |
| 86.0 | 0.98277 | 0.98576 | 0.98266 | 0.98534 | 0.98594 | 0.98469 | 0.98586 | 0.98630 | 0.98564 | 0.98651 | 0.98732 |
| 87.0 | 0.98210 | 0.98521 | 0.98199 | 0.98477 | 0.98540 | 0.98411 | 0.98531 | 0.98577 | 0.98509 | 0.98599 | 0.98683 |
| 88.0 | 0.98143 | 0.98466 | 0.98132 | 0.98421 | 0.98485 | 0.98352 | 0.98476 | 0.98525 | 0.98453 | 0.98547 | 0.98634 |
| 89.0 | 0.98076 | 0.98411 | 0.98065 | 0.98364 | 0.98431 | 0.98293 | 0.98422 | 0.98472 | 0.98398 | 0.98495 | 0.98585 |
| 90.0 | 0.98009 | 0.98356 | 0.97998 | 0.98307 | 0.98377 | 0.98234 | 0.98367 | 0.98419 | 0.98342 | 0.98443 | 0.98536 |
| 91.0 | 0.97942 | 0.98301 | 0.97931 | 0.98251 | 0.98323 | 0.98175 | 0.98312 | 0.98366 | 0.98286 | 0.98391 | 0.98487 |
| 92.0 | 0.97875 | 0.98246 | 0.97863 | 0.98194 | 0.98268 | 0.98116 | 0.98257 | 0.98313 | 0.98231 | 0.98339 | 0.98439 |
| 93.0 | 0.97807 | 0.98190 | 0.97796 | 0.98137 | 0.98214 | 0.98057 | 0.98202 | 0.98260 | 0.98175 | 0.98287 | 0.98390 |
| 94.0 | 0.97740 | 0.98135 | 0.97729 | 0.98080 | 0.98160 | 0.97999 | 0.98147 | 0.98207 | 0.98119 | 0.98235 | 0.98341 |
| 95.0 | 0.97673 | 0.98080 | 0.97662 | 0.98024 | 0.98106 | 0.97940 | 0.98092 | 0.98154 | 0.98063 | 0.98183 | 0.98292 |
| 96.0 | 0.97605 | 0.98025 | 0.97595 | 0.97967 | 0.98051 | 0.97881 | 0.98037 | 0.98101 | 0.98007 | 0.98131 | 0.98243 |
| 97.0 | 0.97538 | 0.97970 | 0.97527 | 0.97910 | 0.97997 | 0.97822 | 0.97982 | 0.98048 | 0.97952 | 0.98079 | 0.98194 |
| 98.0 | 0.97470 | 0.97915 | 0.97460 | 0.97853 | 0.97943 | 0.97763 | 0.97927 | 0.97996 | 0.97896 | 0.98028 | 0.98145 |
| 99.0 | 0.97403 | 0.97859 | 0.97393 | 0.97797 | 0.97888 | 0.97704 | 0.97871 | 0.97943 | 0.97840 | 0.97976 | 0.98096 |
| 100.0 | 0.97335 | 0.97804 | 0.97325 | 0.97740 | 0.97834 | 0.97645 | 0.97816 | 0.97890 | 0.97784 | 0.97924 | 0.98047 |
| 101.0 | 0.97268 | 0.97749 | 0.97258 | 0.97683 | 0.97780 | 0.97587 | 0.97761 | 0.97837 | 0.97728 | 0.97872 | 0.97998 |
| 102.0 | 0.97200 | 0.97694 | 0.97191 | 0.97626 | 0.97725 | 0.97528 | 0.97706 | 0.97784 | 0.97672 | 0.97820 | 0.97949 |
| 103.0 | 0.97132 | 0.97638 | 0.97123 | 0.97569 | 0.97671 | 0.97469 | 0.97651 | 0.97730 | 0.97616 | 0.97768 | 0.97900 |
| 104.0 | 0.97064 | 0.97583 | 0.97056 | 0.97512 | 0.97617 | 0.97410 | 0.97595 | 0.97677 | 0.97560 | 0.97716 | 0.97852 |
| 105.0 | 0.96996 | 0.97528 | 0.96989 | 0.97456 | 0.97562 | 0.97351 | 0.97540 | 0.97624 | 0.97504 | 0.97664 | 0.97803 |
| 106.0 | 0.96929 | 0.97472 | 0.96921 | 0.97399 | 0.97508 | 0.97292 | 0.97485 | 0.97571 | 0.97448 | 0.97612 | 0.97754 |
| 107.0 | 0.96861 | 0.97417 | 0.96854 | 0.97342 | 0.97453 | 0.97233 | 0.97429 | 0.97518 | 0.97392 | 0.97560 | 0.97705 |
| 108.0 | 0.96793 | 0.97362 | 0.96786 | 0.97285 | 0.97399 | 0.97175 | 0.97374 | 0.97465 | 0.97336 | 0.97508 | 0.97656 |
| 109.0 | 0.96725 | 0.97306 | 0.96719 | 0.97228 | 0.97345 | 0.97116 | 0.97318 | 0.97412 | 0.97280 | 0.97456 | 0.97607 |
| 110.0 | 0.96656 | 0.97251 | 0.96651 | 0.97171 | 0.97290 | 0.97057 | 0.97263 | 0.97359 | 0.97223 | 0.97404 | 0.97558 |
| 111.0 | 0.96588 | 0.97196 | 0.96583 | 0.97114 | 0.97236 | 0.96998 | 0.97207 | 0.97306 | 0.97167 | 0.97352 | 0.97509 |
| 112.0 | 0.96520 | 0.97140 | 0.96516 | 0.97058 | 0.97181 | 0.96939 | 0.97152 | 0.97253 | 0.97111 | 0.97300 | 0.97460 |
| 113.0 | 0.96452 | 0.97085 | 0.96448 | 0.97001 | 0.97127 | 0.96880 | 0.97096 | 0.97199 | 0.97055 | 0.97248 | 0.97411 |
| 114.0 | 0.96384 | 0.97029 | 0.96381 | 0.96944 | 0.97073 | 0.96821 | 0.97040 | 0.97146 | 0.96998 | 0.97196 | 0.97362 |
| 115.0 | 0.96315 | 0.96974 | 0.96313 | 0.96887 | 0.97018 | 0.96763 | 0.96985 | 0.97093 | 0.96942 | 0.97144 | 0.97313 |
| 116.0 | 0.96247 | 0.96918 | 0.96245 | 0.96830 | 0.96964 | 0.96704 | 0.96929 | 0.97040 | 0.96886 | 0.97092 | 0.97264 |
| 117.0 | 0.96178 | 0.96863 | 0.96178 | 0.96773 | 0.96909 | 0.96645 | 0.96873 | 0.96987 | 0.96830 | 0.97040 | 0.97215 |
| 118.0 | 0.96110 | 0.96807 | 0.96110 | 0.96716 | 0.96855 | 0.96586 | 0.96818 | 0.96933 | 0.96773 | 0.96988 | 0.97166 |
| 119.0 | 0.96041 | 0.96752 | 0.96042 | 0.96659 | 0.96800 | 0.96527 | 0.96762 | 0.96880 | 0.96717 | 0.96936 | 0.97117 |
| 120.0 | 0.95973 | 0.96696 | 0.95974 | 0.96602 | 0.96746 | 0.96468 | 0.96706 | 0.96827 | 0.96660 | 0.96884 | 0.97068 |
| 121.0 | 0.95904 | 0.96641 | 0.95906 | 0.96546 | 0.96691 | 0.96409 | 0.96650 | 0.96774 | 0.96604 | 0.96832 | 0.97019 |
| 122.0 | 0.95836 | 0.96585 | 0.95839 | 0.96489 | 0.96637 | 0.96350 | 0.96594 | 0.96720 | 0.96548 | 0.96780 | 0.96970 |
| 123.0 | 0.95767 | 0.96529 | 0.95771 | 0.96432 | 0.96582 | 0.96292 | 0.96538 | 0.96667 | 0.96491 | 0.96728 | 0.96921 |
| 124.0 | 0.95698 | 0.96474 | 0.95703 | 0.96375 | 0.96528 | 0.96233 | 0.96483 | 0.96614 | 0.96435 | 0.96676 | 0.96872 |
| 125.0 | 0.95629 | 0.96418 | 0.95635 | 0.96318 | 0.96473 | 0.96174 | 0.96427 | 0.96560 | 0.96378 | 0.96624 | 0.96823 |
| 126.0 | 0.95560 | 0.96362 | 0.95567 | 0.96261 | 0.96418 | 0.96115 | 0.96371 | 0.96507 | 0.96321 | 0.96572 | 0.96773 |
| 127.0 | 0.95492 | 0.96307 | 0.95499 | 0.96205 | 0.96364 | 0.96056 | 0.96315 | 0.96453 | 0.96265 | 0.96520 | 0.96724 |
| 128.0 | 0.95423 | 0.96251 | 0.95431 | 0.96148 | 0.96309 | 0.95997 | 0.96258 | 0.96400 | 0.96208 | 0.96468 | 0.96675 |
| 129.0 | 0.95354 | 0.96195 | 0.95363 | 0.96091 | 0.96255 | 0.95938 | 0.96202 | 0.96347 | 0.96152 | 0.96416 | 0.96626 |
| 130.0 | 0.95284 | 0.96140 | 0.95295 | 0.96034 | 0.96200 | 0.95880 | 0.96146 | 0.96293 | 0.96095 | 0.96364 | 0.96577 |
| 131.0 | 0.95215 | 0.96084 | 0.95227 | 0.95977 | 0.96146 | 0.95821 | 0.96090 | 0.96240 | 0.96038 | 0.96312 | 0.96528 |
| 132.0 | 0.95146 | 0.96028 | 0.95159 | 0.95921 | 0.96091 | 0.95762 | 0.96034 | 0.96186 | 0.95982 | 0.96260 | 0.96479 |
| 133.0 | 0.95077 | 0.95972 | 0.95091 | 0.95864 | 0.96036 | 0.95703 | 0.95978 | 0.96133 | 0.95925 | 0.96208 | 0.96430 |
| 134.0 | 0.95008 | 0.95917 | 0.95023 | 0.95807 | 0.95982 | 0.95644 | 0.95921 | 0.96079 | 0.95868 | 0.96156 | 0.96381 |
| 135.0 | 0.94939 | 0.95861 | 0.94955 | 0.95750 | 0.95927 | 0.95585 | 0.95865 | 0.96026 | 0.95812 | 0.96104 | 0.96332 |
| 136.0 | 0.94869 | 0.95805 | 0.94887 | 0.95694 | 0.95872 | 0.95526 | 0.95809 | 0.95972 | 0.95755 | 0.96052 | 0.96283 |


[^0]:    ${ }^{1}$ This test method is under the jurisdiction of ASTM Committee D16 on Aromatic, Industrial, Specialty and Related Chemicals and is the direct responsibility of Subcommittee D16.01 on Benzene, Toluene, Xylenes, Cyclohexane and Their Derivatives.

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[^1]:    ${ }^{2}$ For referenced ASTM standards, visit the ASTM website, www.astm.org, or contact ASTM Customer Service at service@astm.org. For Annual Book of ASTM Standards volume information, refer to the standard's Document Summary page on the ASTM website.

    3 "Selected Values of Properties of Hydrocarbons and Related Compounds," prepared by American Petroleum Institute Research Project 44 at the Chemical Thermodynamics Center, Department of Chemistry, Texas A\&M, College Station, TX.
    ${ }^{4}$ Available from National Institute of Standards and Technology (NIST), 100 Bureau Dr., Stop 1070, Gaithersburg, MD 20899-1070, http://www.nist.gov.

