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Industrial-process control valves - Part 2-1: Flow capacity - Sizing equations for fluid flow under installed conditions (IEC 60534-2-1:2011)

Stellventile für die Prozessregelung Teil 2-1: Durchflusskapazität Bemessungsgleichungen für Fluide unter Betriebsbedingungen (IEC 60534-2-1:2011)

Vannes de régulation des processus industriels -2 Partie 2-1: Capacité d'écoulement -Equations de dimensionnement pour l'écoulement/des fluides dans les conditions d'installation (CEI 60534-2-1:2014) c430bb33/sist-en-60534-2-1-2011

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English version

Industrial-process control valves -Part 2-1: Flow capacity -Sizing equations for fluid flow under installed conditions (IEC 60534-2-1:2011)

Vannes de régulation des processus industriels -Partie 2-1: Capacité d'écoulement -Equations de dimensionnement pour l'écoulement des fluides dans les conditions d'installation (CEI 60534-2-1:2011) Stellventile für die Prozessregelung -Teil 2-1: Durchflusskapazität -Bemessungsgleichungen für Fluide unter Betriebsbedingungen (IEC 60534-2-1:2011)

(CEI 60534-2-1:2011) iTeh STANDARD PREVIEW (standards.iteh.ai)

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CENELEC

European Committee for Electrotechnical Standardization Comité Européen de Normalisation Electrotechnique Europäisches Komitee für Elektrotechnische Normung

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Foreword

The text of document 65B/783/FDIS, future edition 2 of IEC 60534-2-1, prepared by SC 65B, Devices & process analysis, of IEC TC 65, Industrial-process measurement, control and automation, was submitted to the IEC-CENELEC parallel vote and was approved by CENELEC as EN 60534-2-1 on 2011-05-04.

This European Standard supersedes EN 60534-2-1:1998.

EN 60534-2-1:2011 includes the following significant technical changes with respect to EN 60534-2-1:1998:

- the same fundamental flow model, but changes the equation framework to simplify the use of the standard by introducing the notion of Δp_{sizing} ;
- changes to the non-turbulent flow corrections and means of computing results;
- multi-stage sizing as an Annex.

Attention is drawn to the possibility that some of the elements of this document may be the subject of patent rights. CEN and CENELEC shall not be held responsible for identifying any or all such patent rights.

The following dates were fixed:

 latest date by which the EN has to be implemented at national level by publication of an identical ARD PREV (dop) 2012-02-04
latest date by which the national standards conflicting with the EN have to be withdrawn (dow) 2014-05-04 <u>SIST EN 60534-2-12011</u>
Annex ZA has been added by CENELEC talog/standards/sist/a3615b03-2b10-4d43-a04a-8af5c430bb33/sist-en-60534-2-1-2011

Endorsement notice

The text of the International Standard IEC 60534-2-1:2011 was approved by CENELEC as a European Standard without any modification.

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Annex ZA

(normative)

Normative references to international publications with their corresponding European publications

The following referenced documents are indispensable for the application of this document. For dated references, only the edition cited applies. For undated references, the latest edition of the referenced document (including any amendments) applies.

NOTE When an international publication has been modified by common modifications, indicated by (mod), the relevant EN/HD applies.

Publication	Year	Title	<u>EN/HD</u>	<u>Year</u>
IEC 60534-1	2005	Industrial-process control valves - Part 1: Control valve terminology and general considerations	EN 60534-1	2005
IEC 60534-2-3	1997	Industrial-process control valves - Part 2-3: Flow capacity - Test procedures	EN 60534-2-3	1998

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NORME INTERNATIONALE

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INTERNATIONAL ELECTROTECHNICAL COMMISSION

INDUSTRIAL-PROCESS CONTROL VALVES -

Part 2-1: Flow capacity – Sizing equations for fluid flow under installed conditions

FOREWORD

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International Standard IEC 60534-2-1 has been prepared by subcommittee 65B: Measurement and control devices, of IEC technical committee 65: Industrial-process measurement, control and automation.

This second edition cancels and replaces the first edition published in 1998. This edition constitutes a technical revision.

This edition includes the following significant technical changes with respect to the previous edition:

- the same fundamental flow model, but changes the equation framework to simplify the use of the standard by introducing the notion of *∆p_{sizing}*;
- changes to the non-turbulent flow corrections and means of computing results;
- multi-stage sizing as an Annex.

The text of this standard is based on the following documents:

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FDIS	Report on voting
65B/783/FDIS	65B/786/RVD

Full information on the voting for the approval of this standard can be found in the report on voting indicated in the above table.

This publication has been drafted in accordance with the ISO/IEC Directives, Part 2.

A list of all the parts of the IEC 60534 series, under the general title *Industrial-process control valves*, can be found on the IEC website.

The committee has decided that the contents of this publication will remain unchanged until the stability date indicated on the IEC web site under "http://webstore.iec.ch" in the data related to the specific publication. At this date, the publication will be

- reconfirmed,
- withdrawn,
- replaced by a revised edition, or
- amended.

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INDUSTRIAL-PROCESS CONTROL VALVES -

Part 2-1: Flow capacity – Sizing equations for fluid flow under installed conditions

1 Scope

This part of IEC 60534 includes equations for predicting the flow of compressible and incompressible fluids through control valves.

The equations for incompressible flow are based on standard hydrodynamic equations for Newtonian incompressible fluids. They are not intended for use when non-Newtonian fluids, fluid mixtures, slurries or liquid-solid conveyance systems are encountered. The equations for incompressible flow may be used with caution for non-vaporizing multi-component liquid mixtures. Refer to Clause 6 for additional information.

At very low ratios of pressure differential to absolute inlet pressure $(\Delta p/p_1)$, compressible fluids behave similarly to incompressible fluids. Under such conditions, the sizing equations for compressible flow can be traced to the standard hydrodynamic equations for Newtonian incompressible fluids. However, increasing values of $\Delta p/p_1$ result in compressibility effects which require that the basic equations be modified by appropriate correction factors. The equations for compressible fluids are for use with ideal gas or vapor and are not intended for use with multiphase streams such as gas-liquid, vapor-liquid or gas-solid mixtures. Reasonable accuracy can only be maintained when the specific heat ratio, γ , is restricted to the range 1,08 < γ < 1,65. Refer to Clause 7.2 for more information.

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For compressible fluid applications, this standard is valid for values with $x_T \le 0.84$ (see Table D.2). For values with $x_T > 0.84$ (e.g. some multistage values), greater inaccuracy of flow prediction can be expected.

Reasonable accuracy can only be maintained for control valves if:

$$\frac{C}{N_{18}d^2} < 0,047$$

Note that while the equation structure utilized in this document departs radically from previous versions of the standard, the basic technology is relatively unchanged. The revised equation format was adopted to simplify presentation of the various equations and improve readability of the document.

2 Normative references

The following referenced documents are indispensable for the application of this document. For dated references, only the edition cited applies. For undated references, the latest edition of the referenced document (including any amendments) applies.

IEC 60534-1:2005, Industrial-process control valves – Part 1: Control valve terminology and general considerations

IEC 60534-2-3:1997, Industrial-process control valves – Part 2-3: Flow capacity – Test procedures

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3 Terms and definitions

For the purposes of this document, the terms and definitions given in IEC 60534-1, and the following apply.

3.1

valve style modifier

the ratio of the hydraulic diameter of a single flow passage to the diameter of a circular orifice, the area of which is equivalent to the sum of areas of all identical flow passages at a given travel. It should be stated by the manufacturer as a function of travel (see Annex A).

3.2

standard volumetric flowrates

compressible fluid volumetric flow rates in cubic metres per hour, identified by the symbol $Q_{\rm S}$, refer to either

- a) *Standard* conditions, which is an absolute pressure of 1 013,25 mbar and a temperature of 288,6 K, or
- b) *Normal* conditions, which is an absolute pressure of 1 013,25 mbar and a temperature of 273 K.

Numerical constants for the flow equations are provided for both conventions (see Table 1).

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4 Symbols

Symbo I	Description	Unit
С	Flow coefficient (K_v , C_v)	Various (see IEC 60534-1) (see Note 4)
d	Nominal valve size	mm
D	Internal diameter of the piping	mm
D ₁	Internal diameter of upstream piping	mm
D ₂	Internal diameter of downstream piping	mm
Do	Orifice diameter	mm
F _d	Valve style modifier (see Annex A)	Dimensionless (see Note 4)
F_{F}	Liquid critical pressure ratio factor	Dimensionless
FL	Liquid pressure recovery factor of a control valve without attached fittings	Dimensionless (see Note 4)
F_{LP}	Combined liquid pressure recovery factor and piping geometry factor of a control valve with attached fittings	Dimensionless
F _P	Piping geometry factor	Dimensionless
F _R	Reynolds number factor	Dimensionless
F_{γ}	Specific heat ratio factor STANDARD PREVIEW	Dimensionless
М	Molecular mass of flowing fluistandards.iteh.ai)	kg/kmol
N	Numerical constants (see Table 1)	Various (see Note 1)
<i>p</i> ₁	Inlet absolute static pressure measured at point A (See Figure 1) https://standards.iten.avcatalog/standards/stst/a3615b03-2b10-4d43-	a04a- kPa or bar (see Note 2)
<i>p</i> ₂	Outlet absolute static pressure measured at point B)(see Figure 1)	kPa or bar
pc	Absolute thermodynamic critical pressure	kPa or bar
pr	Reduced pressure (p_1/p_c)	Dimensionless
ρ_{v}	Absolute vapour pressure of the liquid at inlet temperature	kPa or bar
∆ p _{actual}	Differential pressure between upstream and downstream pressure taps $(P_1 - P_2)$	kPa or bar
$\varDelta p_{choked}$	Computed value of limiting pressure differential for incompressible flow	kPa or bar
Δp_{sizing}	Value of pressure differential used in computing flow or required flow coefficient for incompressible flows	kPa or bar
Q	Actual volumetric flow rate	m ³ /h
Qs	Standard volumetric flow rate (see definition 3.2)	m ³ /h
Re _v	Valve Reynolds number	Dimensionless
<i>T</i> ₁	Inlet absolute temperature	К
T_{c}	Absolute thermodynamic critical temperature	К
T _r	Reduced temperature (T_1/T_c)	Dimensionless
t _s	Absolute reference temperature for standard cubic metre	К
W	Mass flow rate	kg/h
x	Ratio of actual pressure differential to inlet absolute pressure (${\Delta}P/P_1$)	Dimensionless
X _{choked}	Choked pressure drop ratio for compressible flow	Dimensionless
X sizing	Value of pressure drop ratio used in computing flow or required flow coefficient for compressible flows	Dimensionless

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Symbo I	Description	Unit
x _T	Pressure differential ratio factor of a control valve without attached fittings at choked flow	Dimensionless (see Note 4)
x _{TP}	Pressure differential ratio factor of a control valve with attached fittings at choked flow	Dimensionless
Y	Expansion factor	Dimensionless
<i>Z</i> ₁	Compressibility factor at inlet conditions	Dimensionless
V	Kinematic viscosity	m ² /s (see Note 3)
ρ_1	Density of fluid at p_1 and T_1	kg/m³
ρ_1/ρ_0	Relative density (ρ_1/ρ_0 = 1,0 for water at 15 °C)	Dimensionless
γ	Specific heat ratio	Dimensionless
ζ	Velocity head loss coefficient of a reducer, expander or other fitting attached to a control valve or valve trim	Dimensionless
51	Upstream velocity head loss coefficient of fitting	Dimensionless
ζ2	Downstream velocity head loss coefficient of fitting	Dimensionless
ζв1	Inlet Bernoulli coefficient	Dimensionless
ζ _{B2}	Outlet Bernoulli coefficient	Dimensionless
NOTE 1 To determine the units for the numerical constants, dimensional analysis may be performed on the appropriate equations using the units given in Table 1.		
NOTE 2 1 bar = 10 ² kPa = 10 ⁵ Pa (standards.iteh.ai)		
NOTE 3 1 centistoke = 10^{-6} m ² /s		
NOTE 4 These values are travel-related and should be stated by the manufacturer.		
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5 Installation

In many industrial applications, reducers or other fittings are attached to the control valves. The effect of these types of fittings on the nominal flow coefficient of the control valve can be significant. A correction factor is introduced to account for this effect. Additional factors are introduced to take account of the fluid property characteristics that influence the flow capacity of a control valve.

In sizing control valves, using the relationships presented herein, the flow coefficients calculated are assumed to include all head losses between points A and B, as shown in Figure 1.