



Designation: D4692 – 01 (Reapproved 2006)<sup>e1</sup>

## Standard Practice for Calculation and Adjustment of Sulfate Scaling Salts (CaSO<sub>4</sub>, SrSO<sub>4</sub>, and BaSO<sub>4</sub>) for Reverse Osmosis and Nanofiltration<sup>1</sup>

This standard is issued under the fixed designation D4692; the number immediately following the designation indicates the year of original adoption or, in the case of revision, the year of last revision. A number in parentheses indicates the year of last reapproval. A superscript epsilon ( $\epsilon$ ) indicates an editorial change since the last revision or reapproval.

<sup>e1</sup> NOTE—Sections 2 and 3.1 were updated editorially in February 2007.

### 1. Scope

1.1 This practice covers the calculation and adjustment of calcium, strontium, and barium sulfates for the concentrate stream of a reverse osmosis or nanofiltration system. The calculations are used to determine the need for scale control in the operation and design of reverse osmosis and nanofiltration installations. This practice is applicable for all types of reverse osmosis devices (tubular, spiral wound, and hollow fiber) and nanofiltration devices.

1.2 This practice is applicable to both brackish waters and seawaters.

### 2. Referenced Documents

#### 2.1 ASTM Standards:<sup>2</sup>

D511 Test Methods for Calcium and Magnesium In Water

D516 Test Method for Sulfate Ion in Water

D1129 Terminology Relating to Water

D3352 Test Method for Strontium Ion in Brackish Water, Seawater, and Brines

D4194 Test Methods for Operating Characteristics of Reverse Osmosis and Nanofiltration Devices

D4195 Guide for Water Analysis for Reverse Osmosis and Nanofiltration Application

D4382 Test Method for Barium in Water, Atomic Absorption Spectrophotometry, Graphite Furnace

D6161 Terminology Used for Microfiltration, Ultrafiltration, Nanofiltration and Reverse Osmosis Membrane Processes

### 3. Terminology

3.1 *Definitions*—For definitions of terms used in this practice, refer to Terminology D1129 and D6161.

<sup>1</sup> This practice is under the jurisdiction of ASTM Committee D19 on Water and is the direct responsibility of Subcommittee D19.08 on Membranes and Ion Exchange Materials.

Current edition approved Dec. 15, 2006. Published February 2007. Originally approved in 1987. Last previous edition approved in 2001 as D4692 – 01. DOI: 10.1520/D4692-01R06E01.

<sup>2</sup> For referenced ASTM standards, visit the ASTM website, [www.astm.org](http://www.astm.org), or contact ASTM Customer Service at [service@astm.org](mailto:service@astm.org). For *Annual Book of ASTM Standards* volume information, refer to the standard's Document Summary page on the ASTM website.

#### 3.2 *Definitions of Terms Specific to This Standard:*

3.2.1 For definitions of terms relating to reverse osmosis, refer to Test Methods D4194.

### 4. Summary of Practice

4.1 This practice consists of calculating the potential for scaling by CaSO<sub>4</sub>, SrSO<sub>4</sub>, and BaSO<sub>4</sub> in a reverse osmosis or nanofiltration concentrate stream from the concentration of Ca<sup>++</sup>, Sr<sup>++</sup>, Ba<sup>++</sup>, and SO<sub>4</sub><sup>=</sup> in the feed solution and the recovery of the reverse osmosis or nanofiltration system.

4.2 This practice also presents techniques to eliminate scaling by decreasing the recovery, by decreasing the Ca<sup>++</sup>, Sr<sup>++</sup>, and Ba<sup>++</sup> concentrations in the feed water, and by addition of scale inhibitors.

### 5. Significance and Use

5.1 In the design and operation of reverse osmosis and nanofiltration installations, it is important to predict the CaSO<sub>4</sub>, SrSO<sub>4</sub>, and BaSO<sub>4</sub> scaling properties of the concentrate stream. Because of the increase in total dissolved solids and the increase in concentration of the scaling salts, the scaling properties of the concentrate stream will be quite different from those of the feed solution. This practice permits the calculation of the scaling potential for the concentrate stream from the feed water analyses and the reverse osmosis or nanofiltration operating parameters.

5.2 Scaling by CaSO<sub>4</sub>, SrSO<sub>4</sub>, and BaSO<sub>4</sub> will adversely affect the reverse osmosis or nanofiltration performance. This practice gives various procedures for the prevention of scaling.

### 6. Procedure

6.1 Determine the concentrations of Ca<sup>++</sup>, Sr<sup>++</sup>, Ba<sup>++</sup>, and SO<sub>4</sub><sup>=</sup> in the feed stream in accordance with Test Methods D511, D3352, D4382, and D516, respectively.

NOTE 1—If H<sub>2</sub>SO<sub>4</sub> is used for control of CaCO<sub>3</sub> scale, measure the SO<sub>4</sub><sup>=</sup> after acid addition.

6.2 Determine the concentration of all major ions using the appropriate methods given in Guide D4195. At a minimum, the concentrations of Mg<sup>++</sup>, Na<sup>+</sup>, HCO<sub>3</sub><sup>=</sup>, and Cl<sup>=</sup> must be determined.

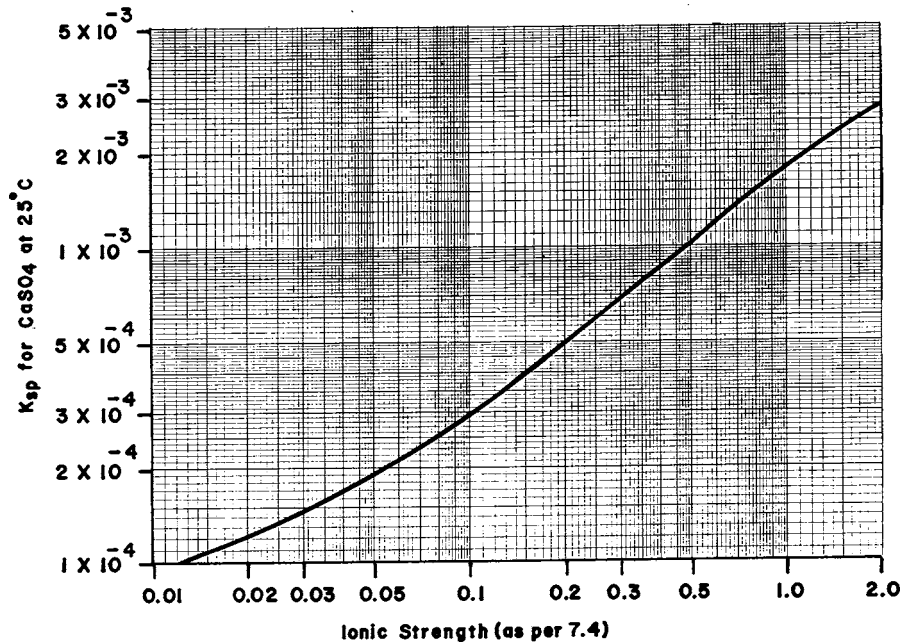


FIG. 1  $K_{sp}$  for  $\text{CaSO}_4$  versus Ionic Strength

## 7. Calculation

7.1 Calculate the calcium concentration in the concentrate stream from the calcium concentration in the feed solution, from the recovery of the reverse osmosis or nanofiltration system, and from the calcium ion passage as follows:

$$Ca_c = Ca_f \times \frac{1 - Y(SP_{Ca})}{1 - Y}$$

where:

- $Ca_c$  = calcium ion concentration in concentrate, mg/L,
- $Ca_f$  = calcium ion concentration in feed, mg/L,
- $Y$  = recovery of the reverse osmosis system, expressed as a decimal, and
- $SP_{Ca}$  = calcium ion passage, expressed as a decimal.

NOTE 2— $SP_{Ca}$  can be obtained from the supplier of the reverse osmosis or nanofiltration system. For most reverse osmosis and nanofiltration devices,  $SP_{Ca}$  can be considered to be zero, in which case the equation simplifies to:

$$Ca_c = Ca_f \times \frac{1}{1 - Y}$$

This assumption will introduce only a small error.

7.2 Calculate the  $\text{SO}_4^{2-}$  concentration in the concentrate stream from the  $\text{SO}_4^{2-}$  concentration in the feed solution, from the recovery of the reverse osmosis or nanofiltration system, and from the sulfate ion passage by using the appropriate substitutions in the equation given in 7.1. The simplified equation can be used.

7.3 Calculate the concentration of the major ions in the concentrate stream using the appropriate substitutions in the equation given in 7.1. The simplified equation can be used.

7.4 Calculate the ionic strength of the concentrate stream as follows:

$$I_c = \frac{1}{2} \sum \bar{m}_i Z_i^2$$

where:

- $I_c$  = ionic strength of concentrate stream,
- $\bar{m}_i$  = molal concentration of ion,  $i$  (moles/1000 g of water) in the concentrate stream, and
- $Z_i$  = ionic charge of ion,  $i$ .

NOTE 3—The molal concentration is calculated as follows:

$$m_i = \frac{C_i}{1000 MW_i \left[ \frac{10^6 - TDS}{10^6} \right]} = \frac{1000 C_i}{MW_i (10^6 - TDS)}$$

where:

- $C_i$  = concentration of ion,  $i$ , in concentrate stream, mg/L,
- $MW_i$  = molecular weight of ion,  $i$ , and
- $TDS$  = total dissolved solids in concentrate stream, mg/L.

7.5 Calculate the ion product ( $IP_c$ ) for  $\text{CaSO}_4$  in the concentrate stream as follows:

$$IP_c = ({}^m\text{Ca}^{++})_c ({}^m\text{SO}_4^{--})_c$$

where:

- $({}^m\text{Ca}^{++})_c$  =  $M \text{Ca}^{++}$  in concentrate, mol/L and
- $({}^m\text{SO}_4^{--})_c$  =  $M \text{SO}_4^{--}$  in concentrate, mol/L.

7.6 Compare  $IP_c$  for  $\text{CaSO}_4$  with the solubility product ( $K_{sp}$ ) of  $\text{CaSO}_4$  at the ionic strength of the concentrate stream (Fig. 1).<sup>3</sup> If  $IP_c > K_{sp}$ ,  $\text{CaSO}_4$  scaling will occur and adjustment is required.

NOTE 4—Some suppliers use a safety factor. Check with the supplier of the reverse osmosis or nanofiltration device to determine if some fraction of the  $K_{sp}$ , for example 0.8  $K_{sp}$ , should be used to compare with  $IP_c$ .

<sup>3</sup> Marshall, W. L. and Slusher, R., "Solubility to 200°C of Sulfate and its Hydrates in Sea Water and Saline Water Concentrates and Temperature, Concentration Limits," *Journal of Chemical and Engineering Data*, Vol 13, No. 1, 1968, p. 83.