

SLOVENSKI STANDARD oSIST prEN ISO 3405:2018

01-januar-2018

Naftni in sorodni proizvodi iz naravnih ali sintetičnih virov - Določevanje destilacijskih značilnosti pri atmosferskem tlaku (ISO/DIS 3405:2017)

Petroleum and related products from natural or synthetic sources - Determination of distillation characteristics at atmospheric pressure (ISO/DIS 3405:2017)

Mineralölerzeugnisse und verwandte Produkte mit natürlichem oder synthetischem Ursprung - Bestimmung des Destillationsverlaufes bei Atmosphärendruck (ISO/DIS 3405:2017)

<u>IST EN ISO 3405:2019</u>

Pétrole et produits dérivés à partir de sources naturelle ou synthétique - Détermination des caractéristiques de distillation à pression atmosphérique (ISO/DIS 3405:2017)

Ta slovenski standard je istoveten z: prEN ISO 3405

ICS:

75.080 Naftni proizvodi na splošno

Petroleum products in general

oSIST prEN ISO 3405:2018

en

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DRAFT INTERNATIONAL STANDARD ISO/DIS 3405

ISO/TC 28

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Petroleum and related products from natural or synthetic sources — Determination of distillation characteristics at atmospheric pressure

Pétrole et produits dérivés à partir de sources naturelle ou synthétique — Détermination des caractéristiques de distillation à pression atmosphérique

ICS: 75.080

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Foreword

ISO (the International Organization for Standardization) is a worldwide federation of national standards bodies (ISO member bodies). The work of preparing International Standards is normally carried out through ISO technical committees. Each member body interested in a subject for which a technical committee has been established has the right to be represented on that committee. International organizations, governmental and non-governmental, in liaison with ISO, also take part in the work. ISO collaborates closely with the International Electrotechnical Commission (IEC) on all matters of electrotechnical standardization.

The procedures used to develop this document and those intended for its further maintenance are described in the ISO/IEC Directives, Part 1. In particular the different approval criteria needed for the different types of ISO documents should be noted. This document was drafted in accordance with the editorial rules of the ISO/IEC Directives, Part 2 (see www.iso.org/directives).

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For an explanation on the meaning of ISO specific terms and expressions related to conformity assessment, as well as information about ISO's adherence to the World Trade Organization (WTO) principles in the Technical Barriers to Trade (TBT) see the following URL: www.iso.org/iso/foreword.html.

The committee responsible for this document is ISO/TC 28, *Petroleum and related products, fuels and lubricants from natural or synthetic sources*. This International Standard includes content and data, with permission of ASTM International, from ASTM D86^[1], copyright ASTM International.

This fifth edition cancels and replaces the fourth edition (ISO 3405:2010). The following updates have been taken into account:

- extension of the scope to synthetic and biological products in general and to automotive petrol-ethanol blends and to B30 biodiesel specifically;
- the procedure has been aligned with ASTM D86 [1] and ASTM International has granted usage of its precision data on 5 July 2017;
- update of the precision (for automated apparatus) for Groups 1, 2, and 3, with the slope based precision obtained from a 2010 Interlaboratory Study [2];
- for T95, Group 4 has a valid range now of 260 °C to 360 °C and an updated precision, as review of a 2006 Interlaboratory Study revealed the absence of some Group 4 samples having boiling point near 360 °C, as well final boiling points are above;
- introduction of a solution for the replacement of mercury-in-glass thermometers.

DRAFT INTERNATIONAL STANDARD

Petroleum and related products from natural or synthetic sources — Determination of distillation characteristics at atmospheric pressure

WARNING — The use of this Standard can involve hazardous materials, operations and equipment. This Standard does not purport to address all of the safety problems associated with its use. It is the responsibility of users of this standard to take appropriate measures to ensure the safety and health of personnel prior to the application of the standard, and fulfil statutory and regulatory requirements for this purpose.

1 Scope

This document specifies a laboratory method for the determination of the distillation characteristics of light and middle distillates derived from petroleum and related products of synthetic or biological origin with initial boiling points above 0 °C and end-points below approximately 400 °C, utilizing either manual or automated equipment. Light distillates are typically; automotive engine petrol, automotive engine ethanol fuel blends with up to 85 % (*V*/*V*) ethanol, and aviation petrol. Middle distillates are typically; aviation turbine fuel, kerosene, diesel, diesel with up to 30 % (*V*/*V*) FAME, burner fuel, and marine fuels that have no appreciable quantities of residua.

NOTE For the purposes of this document, the term "% (*V/V*)" is used to represent the volume fraction of a material.

The distillation (volatility) characteristics of hydrocarbons and related products of synthetic or biological origin have an important effect on their safety and performance, especially in the case of fuels and solvents. The boiling range gives important information on composition and behaviour during storage and use, and the rate of evaporation is an important factor in the application of many solvents. Limiting values to specified distillation characteristics are applied to most distillate petroleum product and liquid fuel specifications in order to control end-use performance and to regulate the formation of vapours which may form explosive mixtures with air, or otherwise escape into the atmosphere as emissions (VOC).

2 Normative references

The following referenced documents are indispensable for the application of this document. For dated references, only the edition cited applies. For undated references, the latest edition of the referenced document (including any amendments) applies.

ISO 918, Volatile organic liquids for industrial use — Determination of distillation characteristics

ISO 3170, Petroleum liquids — Manual sampling

ISO 3171, Petroleum liquids — Automatic pipeline sampling

ISO 4259, Petroleum products — Determination and application of precision data in relation to methods of test

ISO 4788, Laboratory glassware — Graduated measuring cylinders

3 Terms and definitions

For the purposes of this document, the following terms and definitions apply.

3.1

decomposition point

thermometer reading (corrected) which coincides with the first indications of thermal decomposition of the liquid in the flask

NOTE 1 to entry: Characteristic indications of thermal decomposition are an evolution of fumes and erratic thermometer readings which usually show a decided decrease after any attempt has been made to adjust the heat.

3.2

dry point

thermometer reading (corrected) that is observed at the instant the last drop of liquid evaporates from the lowest point in the flask; any drops or film of liquid on the side of the flask or on the thermometer are disregarded

NOTE 1 to entry: The end-point (final boiling point), rather than the dry point is intended for general use. The dry point can be reported in connection with special purpose naphthas, such as those used in the paint industry. Also, it is substituted for the end-point (final boiling point) whenever the sample is of such a nature that the precision of the end-point cannot consistently meet the precision requirements given in Clause 13 or 14.

3.3

end-point

final boiling point

maximum thermometer reading (corrected) obtained during the test

NOTE 1 to entry: This usually occurs after evaporation of all liquid from the bottom of the flask.

3.4

initial boiling point

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thermometer reading (corrected) that is observed at the instant that the first drop of condensate falls from the lower end of the condenser tube 50fce2027069/sist-en-iso-3405-2019

3.5

percent evaporated

sum of the percent recovered and the percent loss

3.6

percent loss

100 minus the total recovery

NOTE 1 to entry: Sometimes called "front-end loss"; this is the amount of uncondensed material lost in the initial stages of the distillation.

3.7

corrected loss

percent loss corrected for barometric pressure

3.8

percent recovered

volume of condensate observed in the receiving cylinder at any point in the distillation, expressed as a percentage of the charge volume, in connection with a simultaneous temperature reading

3.9

percent recovery

maximum percent recovered, as observed in accordance with 9.10

3.10

percent residue

volume of residue measured in accordance with 9.11, and expressed as a percentage of the charge volume

3.11

percent total recovery

combined percent recovery and residue in the flask, as determined in accordance with 10.1

3.12

thermometer reading

temperature recorded by the sensor of the saturated vapour measured in the neck of the flask below the vapour tube, under the specified conditions of this test

3.13

temperature reading

thermometer or temperature-measurement device reading (3.12) which is corrected to 101,3 kPa standard pressure

3.14

emergent stem effect

offset in temperature reading caused by the use of a total immersion mercury-in-glass thermometer in the partial immersion mode

NOTE 1 to entry: The emergent part of the mercury column is at a lower temperature than the immersed portion, resulting in a lower temperature reading than that obtained when the thermometer was completely immersed for calibration.

3.15

temperature lag

offset in temperature reading between a mercury-in-glass thermometer and an electronic temperaturemeasurement device, caused by the different response time of the systems involved

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4 Principle

The sample is assigned into one of four groups based on its composition and expected volatility characteristics, each group defining the apparatus arrangement, condenser temperature and operational variables. A 100 ml test portion is distilled under the specified conditions appropriate to the group into which the sample falls, and systematic observations of thermometer readings and volumes of condensate recovered are made. The volume of the residue in the flask is measured, and the loss on distillation recorded. The thermometer readings are corrected for barometric pressure, and the data are then used for calculations appropriate to the nature of the sample and the specification requirements.

5 Apparatus

5.1 General

Typical assemblies of the manual apparatus are shown in Figures 1 and 2. In addition to the basic components described in Clause 5, automated apparatus also are equipped with a system to measure and automatically record the vapour temperature and the associated recovered volume in the receiving cylinder.

Automated equipment manufactured in 1999 and later shall be equipped with a device to automatically shut down power to the unit and to spray an inert gas or vapour in the chamber where the distillation flask is mounted in the event of fire.

NOTE Some causes of fires are breakage of the distillation flask, electrical shorts, and foaming and spilling of liquid sample through the top opening of the flask.

5.2 Distillation flasks

The distillation flasks shall have a capacity of 125 ml and be constructed of heat-resistant glass, according to the dimensions and tolerances shown in Figure 3.

For tests specifying the dry point, especially selected flasks with bottoms and walls of uniform thickness are recommended.

5.3 Condenser tube and cooling bath

5.3.1 Typical types of condenser and cooling bath are illustrated in Figures 1 and 2.

Other types of apparatus may be used, provided that the test results obtained by their use are such as to correlate with the results obtained with those illustrated, and to satisfy the precision criteria given in Clause 13 or 14.

5.3.2 The condenser shall be made of seamless non-corrosive metal tubing, 560 mm \pm 5 mm in length, with an outside diameter of 14 mm and a wall thickness of 0,8 mm to 0,9 mm.

NOTE Brass or stainless steel are suitable materials.

5.3.3 The condenser shall be set so that 393 mm \pm 3 mm of the tube is in contact with the cooling medium, with 50 mm \pm 3 mm outside the cooling bath at the upper end, and 114 mm \pm 3 mm outside at the lower end. The portion of tube projecting at the upper end shall be set at an angle of 75° +/- 3° to the vertical. The portion of the tube inside the cooling bath shall be either straight or bent in any suitable continuous smooth curve. The average gradient shall be 15° \pm 1° with respect to the horizontal, and no 100 mm section shall have a gradient outside a 15° \pm 3° range. The projecting lower portion of the condenser tube shall be curved downward for a length of 76 mm and the lower end cut off at an acute angle. Provisions shall be made to enable the flow of distillate to run down the side of the receiving cylinder. Figure 4 gives an illustration of the lower end of the condenser tube.

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The flow of distillate down the side of the graduated cylinder may be accomplished either by using a dripdeflector which is inserted in the receiver, or by having the downward length of the condenser tube curve slightly backwards so as to ensure contact with the wall of the receiving cylinder at a point 25 mm to 32 mm below the top of the receiving cylinder when it is in position to receive distillate.

5.3.4 The volume and design of the cooling bath will depend on the cooling medium employed. The cooling capacity of the bath shall be adequate to maintain the required temperature for the desired condenser performance. A single cooling bath may be used for several condenser tubes.

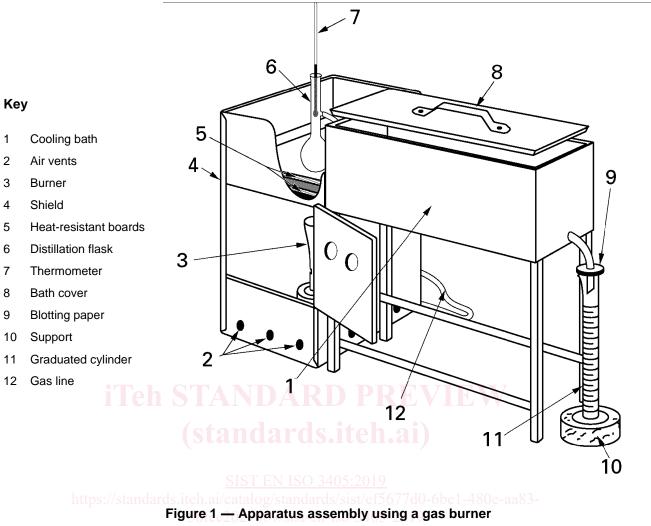
5.4 Metal shield or enclosure for flask (manual apparatus only)

Shields shall be provided to protect the operator from damage from the unit during operation, and to protect the distillation flask from draughts. They shall allow easy access to the distillation during operation, and be provided with at least one window to observe the dry point at the end of the distillation.

NOTE 1 A typical shield for a unit fitted with a gas burner would be 480 mm high, 280 mm long and 200 mm wide, made of sheet metal approximately 0,8 mm in thickness (see Figure 1).

NOTE 2 A typical shield for a unit fitted with an electric heater would be 440 mm high, 200 mm long and 200 mm wide, made of sheet metal approximately 0,8 mm in thickness (see Figure 2).

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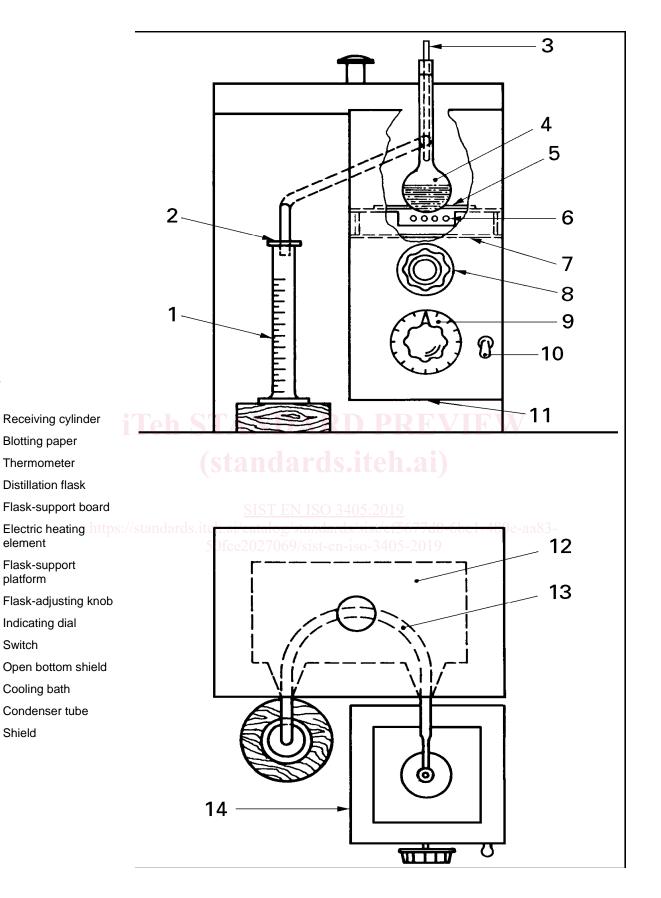


Figure 2 — Apparatus assembly using an electric heater

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Dimensions in millimetres

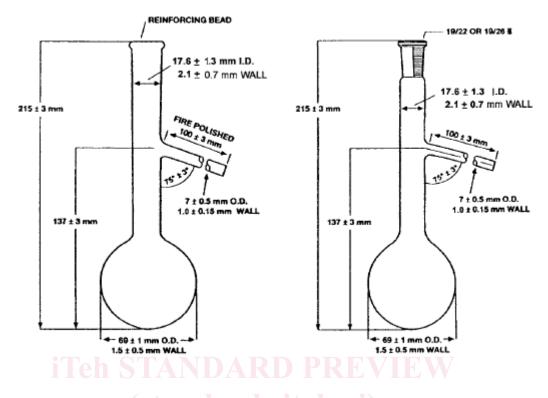
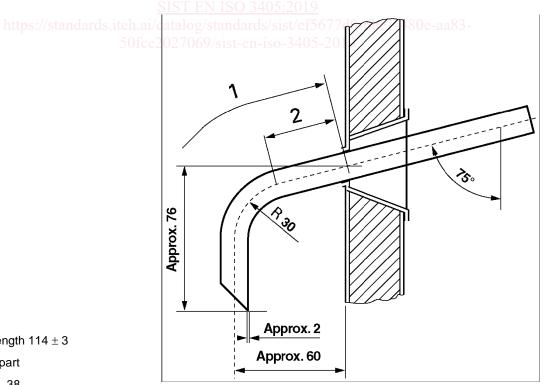


Figure 3 — 125 ml flasks – Alternative neck designs

Dimensions in millimetres



Key

- Total length 114 \pm 3 1
- 2 Linear part Approx. 38

