



**SLOVENSKI STANDARD**  
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**Emisije nepremičnih virov - Določevanje biogenega deleža CO<sub>2</sub> v odpadnih plinih z metodo izračuna**

Stationary source emissions - Determination of the biogenic fraction in CO<sub>2</sub> in stack gas using the balance method

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Émission des sources fixes - Détermination de la fraction biogénique de CO<sub>2</sub> dans les gaz de cheminées en utilisant la méthode des bilans [9](https://standards.iteh.ai/catalog/standards/sist/abee4906-cab7-4df6-9fe2-3249d6eca128/sist-iso-18466-2018)

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**Stationary source emissions —  
Determination of the biogenic  
fraction in CO<sub>2</sub> in stack gas using the  
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*Émission des sources fixes — Détermination de la fraction biogénique  
de CO<sub>2</sub> dans les gaz de cheminées en utilisant la méthode des bilans*

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### Foreword

ISO (the International Organization for Standardization) is a worldwide federation of national standards bodies (ISO member bodies). The work of preparing International Standards is normally carried out through ISO technical committees. Each member body interested in a subject for which a technical committee has been established has the right to be represented on that committee. International organizations, governmental and non-governmental, in liaison with ISO, also take part in the work. ISO collaborates closely with the International Electrotechnical Commission (IEC) on all matters of electrotechnical standardization.

The procedures used to develop this document and those intended for its further maintenance are described in the ISO/IEC Directives, Part 1. In particular the different approval criteria needed for the different types of ISO documents should be noted. This document was drafted in accordance with the editorial rules of the ISO/IEC Directives, Part 2 (see [www.iso.org/directives](http://www.iso.org/directives)).

Attention is drawn to the possibility that some of the elements of this document may be the subject of patent rights. ISO shall not be held responsible for identifying any or all such patent rights. Details of any patent rights identified during the development of the document will be in the Introduction and/or on the ISO list of patent declarations received (see [www.iso.org/patents](http://www.iso.org/patents)).

Any trade name used in this document is information given for the convenience of users and does not constitute an endorsement.

For an explanation on the meaning of ISO specific terms and expressions related to conformity assessment, as well as information about ISO's adherence to the World Trade Organization (WTO) principles in the Technical Barriers to Trade (TBT) see the following URL: [www.iso.org/iso/foreword.html](http://www.iso.org/iso/foreword.html).

The committee responsible for this document is ISO/TC 146, *Air quality*, Subcommittee SC 1, *Stationary source emissions*.

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## Introduction

During the combustion of solid fuels, O<sub>2</sub> is consumed and CO<sub>2</sub> is simultaneously produced. Biogenic and fossil organic matter do not only show strong differences regarding O<sub>2</sub> consumption and CO<sub>2</sub> production, but also differences in their respective calorific value and carbon content are observable.

The balance method can be used when the elementary composition of moisture and ash free biomass and fossil matter present in the fuel used is known and online stack gas composition measurements (O<sub>2</sub> and CO<sub>2</sub>) are available at high accuracy. It will enable online modelling of biomass fossil ratio's in stack gas giving the user the opportunity to control or report that ratio. The generated model data can be verified using the radiocarbon (<sup>14</sup>C) determined biomass fuel ratio. The results obtained using this document will be complementary to the results obtained with ISO 13833. In ISO 13833, the biogenic fraction in stack gas from plants with unknown fuel composition is determined using the <sup>14</sup>C method. If the chemical composition of pure biogenic and fossil matter (contents of C, H, N, S, O referred of moisture and ash free biomass and fossil organic matter, respectively) present in the fuel used is known, the biogenic CO<sub>2</sub> fraction can be calculated utilizing different operating data of the Waste for Energy (WfE) plant. When the chlorine content is sufficiently high, it can be additionally used to optimize the mass balances.

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# Stationary source emissions — Determination of the biogenic fraction in CO<sub>2</sub> in stack gas using the balance method

## 1 Scope

This document enables the determination of the biogenic fraction in CO<sub>2</sub> in stack gas using the balance method. The balance method uses a mathematical model that is based on different operating data of the Waste for Energy (WfE) plant (including stack gas composition) and information about the elementary composition of biogenic and fossil matter present in the fuel used.

NOTE Use only mixed fuels when using the calculation method.

## 2 Normative references

The following documents are referred to in the text in such a way that some or all of their content constitutes requirements of this document. For dated references, only the edition cited applies. For undated references, the latest edition of the referenced document (including any amendments) applies.

ISO 12039, *Stationary source emissions — Determination of carbon monoxide, carbon dioxide and oxygen — Performance characteristics and calibration of automated measuring systems*

EN 14181, *Quality assurance of automated measuring systems*

EN 15259, *Air quality — Measurement of stationary source emissions — Requirements for measurement sections and sites and for the measurement objective, plan and report*

EN 15267-3, *Air quality — Certification of automated measuring systems — Part 3: Performance criteria and test procedures for automated measuring systems for monitoring emissions from stationary sources*

## 3 Terms and definitions

For the purposes of this document, the following terms and definitions apply.

ISO and IEC maintain terminological databases for use in standardization at the following addresses:

- IEC Electropedia: available at <http://www.electropedia.org/>
- ISO Online browsing platform: available at <https://www.iso.org/obp/>

### 3.1

#### **biogenic**

produced in natural processes by living organisms but not fossilized or derived from fossil resources

### 3.2

#### **biomass**

material of biological origin excluding material embedded in geological formation or transformed to fossil

### 3.3

#### **radiocarbon**

radioactive isotope of the element carbon, <sup>14</sup>C, having 8 neutrons, 6 protons, and 6 electrons

### 3.4

#### **sample**

quantity of material, representative of a larger quantity for which the property is to be determined

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## 3.5

**sample preparation**

all the actions taken to obtain representative analyses, *samples* (3.4) or *test portions* (3.6) from the original sample

## 3.6

**test portion**

quantity of material drawn from the test sample (or from the laboratory sample if both are the same) and on which the test or observation is actually carried out

## 3.7

**balance method**

numerical procedure to calculate the fraction of *biogenic* (3.1) matter in waste continuously by solving a set of equations

## 4 Symbols and abbreviated terms

$C^{(f)}$	organic carbon content of the waste fuel derived from operating data (kg C/kg waste fuel)
$\Delta H$	net enthalpy of steam cycle of the Waste for Energy (WfE) plant (MJ/kg)
$J_x$	Jacobian matrix of range $6 \times N$ , with $N$ representing the number of the measured variables
$J_y$	Jacobian matrix of range $6 \times K$ , with $K$ representing the number of the unknown variables
$L_{vap}$	evaporation heat (MJ/kg)
$w_B, w_F, w_{H_2O}, w_I$	mass fractions of moisture and ash free biogenic and fossil matter, water and inert matter (kg/kg waste fuel)
$M_C$	relative molecular mass of carbon (12,010 7 g/mol)
$M_H$	relative molecular mass of hydrogen (1,007 94 g/mol)
$M_O$	relative molecular mass of oxygen (15,999 4 g/mol)
$M_N$	relative molecular mass of nitrogen (14,006 7 g/mol)
$M_S$	relative molecular mass of sulfur (32,065 g/mol)
$M_{gas}$	molecular weight of auxiliary gas fuel (g/mol)
$M_{H_2O}$	molecular weight of water (g/mol)
$O^{(f)}$	oxygen consumption of the waste fuel derived from operating data (mol $O_2$ /kg waste fuel);
$p_v$	vapour pressure of the inlet combustion air (Pa);
$\bar{q}_{LHV_w}$	average lower heating value of the waste feed within a defined period $\Delta t$ (MJ/kg)
$\bar{q}_{LHV_k}$	elemental lower heating value of the combustible fractions ( $k$ is carbon, hydrogen, oxygen, nitrogen and sulfur) (MJ/kg)
$\bar{q}_{LHV_{gas}}$	average lower heating value of the auxiliary gas fuel (MJ/m <sup>3</sup> <sub>273,15 K, 1,013 25 bar</sub> )

$\bar{q}_{\text{LHV, oil}}$	average lower heating value of the auxiliary oil fuel (MJ/kg)
$R_{\text{as}}^*$	specific gas constant for the dry air [287,0558 14 J/(kg K)]
$S_{\text{vap}}$	steam production of the Waste for Energy (WfE) plant within a defined period (kg/ $\Delta t$ )
$\Delta t$	defined time period (arbitrary time unit, e.g. days)
$T_{\text{air}}$	temperature of the inlet combustion air ( $^{\circ}\text{C}$ );
$V_{\text{air}}$	volume of the inlet combustion air ( $\text{m}^3_{273,15 \text{ K}, 1,01325 \text{ bar}}$ );
$V_{\text{fg}}$	dry flue gas volume of the Waste for Energy (WfE) plant within a defined period ( $\text{m}^3_{273,15 \text{ K}, 1,013 25 \text{ bar}/\Delta t$ )
$V_{\text{gas}}$	auxiliary gas fuel volume into the Waste for Energy (WfE) plant within a defined period ( $\text{m}^3_{273,15 \text{ K}, 1,013 25 \text{ bar}/\Delta t$ )
$V_{\text{m}}$	molar volume of ideal gas under standard temperature and pressure (22,414 $\text{dm}^3_{273,15 \text{ K}, 1,013 25 \text{ bar}/\text{mol}$ )
$m_{\text{oil}}$	mass of auxiliary oil fuel into the Waste for Energy (WfE) plant within a defined period (kg/ $\Delta t$ )
$m_{\text{tot}}$	mass of waste into the Waste for Energy (WfE) plant within a defined period (kg/ $\Delta t$ )
$W_{\text{v}}$	vapour mass in the combustion air
$\Sigma W_{\text{s}}$	sum of solid residues (dry substance) of the Waste for Energy (WfE) plant within a defined period (kg/ $\Delta t$ )
$c_{\text{B}}^k$	elemental concentration of the combustible fractions of the biogenic matter (ash and moisture free; $k$ is carbon, hydrogen, oxygen, nitrogen and sulfur) (kg/kg)
$c_{\text{F}}^k$	elemental concentration of the combustible fractions of the fossil organic matter (ash and moisture free; $k$ is carbon, hydrogen, oxygen, nitrogen and sulfur) (kg/kg)
$c_{\text{gas}}^k$	elemental concentration of the auxiliary gas fuel ( $k$ is carbon, hydrogen, oxygen, nitrogen and sulfur) (kg/kg)
$c_{\text{oil}}^k$	elemental concentration of the auxiliary oil fuel ( $k$ is carbon, hydrogen, oxygen, nitrogen and sulfur) (kg/kg)
$x_{\text{O}_2, \text{fg}}, x_{\text{CO}_2, \text{fg}}$	average $\text{O}_2$ and $\text{CO}_2$ content in the dry flue gas of the Waste for Energy (WfE) plant within a defined period $\Delta t$ (vol %)
$x_{\text{O}_2, \text{air}}, x_{\text{CO}_2, \text{air}}$	average $\text{O}_2$ and $\text{CO}_2$ content of dry combustion air of the Waste for Energy (WfE) plant within a defined period $\Delta t$ (vol %)
$x_{\text{H}_2\text{O}}$	average water content in the flue gas of the Waste for Energy (WfE) plant within a defined period $\Delta t$ (vol %)
$\mathbf{x}_{\text{s}}$	vector of $N$ estimated values of the measured variables
$\mathbf{y}_{\text{s}}$	vector of the $K$ unknown variables
$\eta$	energy efficiency of the steam boiler of the Waste for Energy (WfE) plant

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$\varepsilon$	vapour molecular weight/dry air molecular weight (0,621 98)
$\sigma_B^k$	weighted standard deviation for the $k$ -th content of the moisture and ash free biogenic matter present in the waste feed ( $k = C, O, N, H, S$ )
$\sigma_F^k$	weighted standard deviation for the $k$ -th content of the moisture and ash free fossil matter present in the waste feed ( $k = C, O, N, H, S$ )
$\sigma_{wk}$	standard deviation associated to the mass flow of the $k$ -th type of waste
SRF	solid recovered fuel
WfE	waste for energy plant

**5 Requirements****5.1 Input stream parameters**

For the application of the balance method, the following input parameters are required:

- mass of waste feed (within a defined period,  $\Delta t$ );
- mass/volume of auxiliary fuels such as fuel oil or gas (within a defined period,  $\Delta t$ );
- elemental composition of the auxiliary fuels (fuel oil or gas) used (for carbon, hydrogen, oxygen, nitrogen and sulfur);
- total mass and elementary composition of fuels that are either composed of biogenic matter or fossil matter only (e.g. sewage sludge, wood waste);
- elemental composition (probable range) of moisture and ash free biogenic and fossil organic matter (with respect to the content of carbon, hydrogen, oxygen, nitrogen and sulfur) present in the waste feed;
- ratio of different waste types present in the waste feed such as municipal solid waste (MSW) or hospital waste (in case that the waste types are characterized by different elemental composition of biogenic and fossil organic matter);
- energy efficiency of the boiler;
- average temperature of feed water for the boiler (within defined period,  $\Delta t$ );
- amount of air used for the combustion (within defined period,  $\Delta t$ ), not compulsory.

**5.2 Output stream parameters**

For the application of the balance method, the following output stream parameters are required:

- CO<sub>2</sub> concentration in dry flue gas (within defined period,  $\Delta t$ );
- O<sub>2</sub> concentration in dry flue gas (within defined period,  $\Delta t$ );
- flue gas flow volume within defined period,  $\Delta t$  (standardized to 273 K and 101,325 kPa);
- moisture content within defined period,  $\Delta t$ ;
- temperature in stack at measurement point of flue gas flow, within defined period,  $\Delta t$  (in order to convert flue gas flow to standard temperature of 273 K), not compulsory;
- pressure in stack at measurement point of flue gas flow, within defined period,  $\Delta t$  (in order to convert flue gas flow to standard pressure of 101,325 kPa), not compulsory;