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**Safety devices for protection against  
excessive pressure —**

**Part 7:  
Common data**

**AMENDMENT 1**

**iTeh STANDARD PREVIEW**  
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*Dispositifs de sécurité pour protection contre les pressions  
excessives —*

*Partie 7: Données communes*

*ISO 4126-7:2013/Amd 1:2016*

**AMENDEMENT 1**

<https://standards.iteh.ai/catalog/standards/sist/30fa322f-4f76-4105-92d0-c496bbb539c6/iso-4126-7-2013-amd-1-2016>



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Amendment 1 to ISO 4126-7:2013 was prepared by Technical Committee ISO/TC 185, *Safety devices for protection against excessive pressure*.

[ISO 4126-7:2013/Amd 1:2016](https://standards.iteh.ai/catalog/standards/sist/30fa322f-4f76-4105-92d0-c496bbb539c6/iso-4126-7-2013-amd-1-2016)

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# Safety devices for protection against excessive pressure —

## Part 7: Common data

### AMENDMENT 1

*Page 5*

#### **Formula 9**

Delete the equation and substitute:

$$3,948 = \frac{3600}{\sqrt{10^5} \times \sqrt{R}}$$

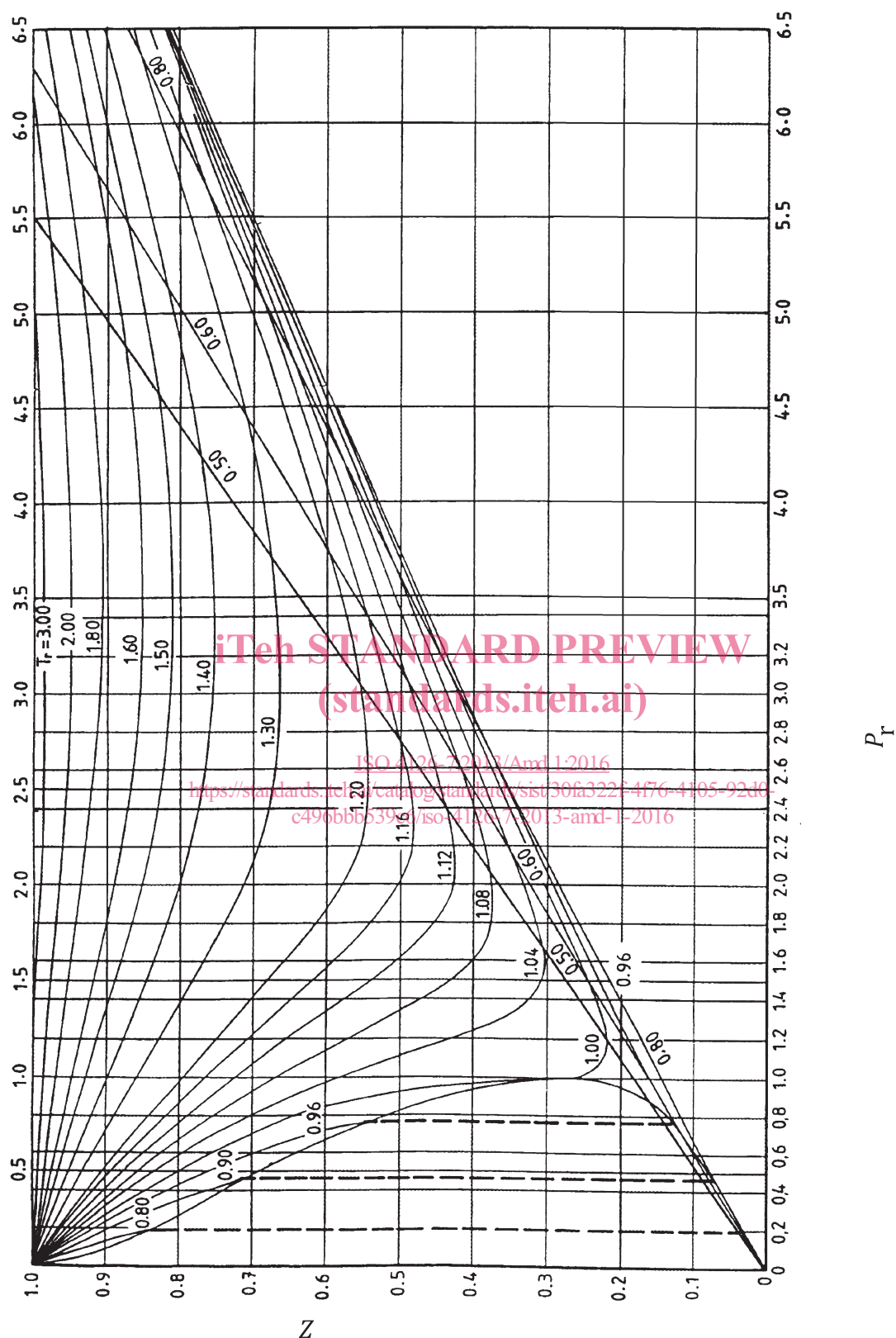
*Page 20*

#### **Figure 1**

Delete the figure and substitute new figure on following page.

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**Key**

- $P_r$  reduced pressure
- $T_r$  reduced temperature
- $Z$  compressibility factor

**Figure 1 — Estimating chart for compressibility factor,  $Z$**

## Clause A.1 Capacity calculations for gaseous media at critical flow (6.3.3.1)

Delete A.1 Example 1 and substitute:

EXAMPLE 1 Calculate the flow area of a safety valve to be used on a vessel holding nitrogen gas with a maximum allowable pressure, PS of 10 bar gauge (1,0 MPa).

Safety valve certified de-rated coefficient of discharge [ $K_{dr}$ ] at 10 % overpressure = 0,87

Molar mass of the gas [ $M$ ] = 28,02

Isentropic exponent of the gas [ $k$ ] = 1,40

Gas relieving temperature = 20 °C

Required gas flow capacity = 18 000 kg/h

Set pressure = 10 bar (1,0 MPa)

Back pressure atmospheric

$T_o = 20 + 273 = 293 \text{ K}$

$p_o = [10 \times 1,1] + 1 = 12 \text{ bar (abs)}$

Since  $\frac{p_b}{p_o} \leq \left( \frac{2}{k+1} \right)^{(k/(k-1))}$  the flow is critical.

The required area,  $A = \frac{Q_m}{p_o C K_{dr} \sqrt{\frac{M}{Z T_o}}}$

$$C = 3,948 \sqrt{1,4 \times \left( \frac{2}{1,4+1} \right)^{(1,4+1)/(1,4-1)}} = 2,7$$

Values for factor C can also be obtained from Table 3.

Compressibility factor, Z, may be estimated from published data.

The calculation involved is as follows:

$$\text{Reduced pressure, } P_r = \frac{p_o}{p_c}$$

where

$p_c$  is the critical pressure = 33,94 bar (abs.) = 3,394 MPa abs (from a thermodynamics handbook).

$$\text{Reduced temperature, } T_r = \frac{T_o}{T_c}$$

where

$T_c$  is the critical temperature = 126,05 K (from a thermodynamics handbook);

$$p_r = 12/33,94 = 0,35;$$

$$T_r = 293/126,05 = 2,32;$$

$$Z = 1,000 \text{ (from Figure 1).}$$

$$A = \frac{18\,000}{12 \times 2,7 \times 0,87 \times \sqrt{\frac{28,02}{1,00 \times 293}}} = 2\,065 \text{ mm}^2$$

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