

ISO/~~FDIS 27913:2023 (E)~~

ISO/TC 265/~~AWG 2~~

Secretariat: SCC

Date: 2024-02-16/05-27

Carbon dioxide capture, transportation and geological storage — Pipeline transportation systems

Captage ~~du dioxyde de carbone~~, transport et stockage géologique ~~du dioxyde de carbone~~ — Systèmes de transport par conduites

FDIS stage

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A model manuscript of a draft International Standard (known as "The Rice Model") is available at

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Foreword

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The procedures used to develop this document and those intended for its further maintenance are described in the ISO/IEC Directives, Part 1. In particular, the different approval criteria needed for the different types of ISO document should be noted. This document was drafted in accordance with the editorial rules of the ISO/IEC Directives, Part 2 (see www.iso.org/directives).

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For an explanation of the voluntary nature of standards, the meaning of ISO specific terms and expressions related to conformity assessment, as well as information about ISO's adherence to the World Trade Organization (WTO) principles in the Technical Barriers to Trade (TBT), see www.iso.org/iso/foreword.html.

This document was prepared by Technical Committee ISO/TC 265, *Carbon dioxide capture, transportation, and geological storage*.

This second edition cancels and replaces the first edition (ISO 27913:2016), which has been technically revised.

The main changes are as follows:

- the entire text has been editorially revised;
- normative references have been updated;
- a ~~chapter~~subclause about CO₂ stream flowrate and impurity measurement has been added;
- the level of impurities ~~was~~has been limited to 5 % and a set of 17 requirements are defined ~~in the normative part to assure~~to ensure CO₂ stream pipeline integrity;
- ~~Annex A~~An informative Annex A ~~was~~has been added to show example compositions of CO₂ streams for gaseous and dense phase CO₂ streams which fulfil the requirements of the normative part of this document;
- ~~Annex D~~Annex D has adopted the latest findings in fracture arrest design.
- ~~Annex F~~Annex F ~~was~~has been added to describe decompression effects on pressure and temperature versus time.

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Introduction

Carbon dioxide (CO₂) capture, [carbon dioxide](#) use (CCU) and [carbon dioxide](#) storage (CCS) have been identified as key abatement technologies for achieving a significant reduction in CO₂ emissions to the atmosphere. Pipelines are likely to be the primary means of transporting CO₂ from the point-of-capture to storage sites (e.g. depleted hydrocarbon formations, deep saline aquifers), or to usage points (e.g. enhanced oil recovery ~~(EOR)~~, or utilization) to avoid its release to the atmosphere. While there is a perception that transporting CO₂ via pipelines does not represent a significant barrier to implementing large-scale CCS, there is significantly less industry experience than there is for hydrocarbon service (e.g. natural gas) and there are a number of issues that need to be adequately understood and the associated risks effectively managed to ensure safe transport of CO₂. In a CCS or CCU context, there is a need for larger CO₂ pipeline systems in more densely populated areas and with CO₂ coming from multiple sources. Also, offshore pipelines for the transportation of CO₂ to offshore storage sites are likely to become common.

The objective of this document is to provide specific requirements and recommendations on certain aspects of safe and reliable design, construction and operation of pipelines intended for the large-scale transportation of CO₂ that are not already covered in existing pipeline standards such as ISO 13623, ASME B31.4, ASME B31.8, EN 1594, AS 2885 or other standards ~~(see listed in the Bibliography)~~. Existing pipeline standards cover many of the issues related to the design and construction of CO₂ pipelines. However, there are some CO₂-specific issues (e.g. fracture arrest, internal corrosion protection, ~~etc.~~) that are not adequately covered in these standards, but is addressed in this ~~standard document~~. The purpose of this document is to cover these issues consistently. Hence, this document is not a standalone standard, but is written to be a supplement to other existing pipeline standards for natural gas or liquids for both onshore and offshore pipelines.

~~Transport of CO₂ via ship, rail and road is not covered in this document.~~

The system boundary (see [Figure 1](#)) between capture and transportation is the point at the inlet valve of the pipeline, where the composition, temperature and pressure of the CO₂ stream is within a certain specified range to meet the requirements for transportation as described in this document.

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|----|--------------------------------------|------|-------------------------------------------------------------------------------------|
| 9 | EO enhanced oil recovery | 1920 | export to other uses than 7, 8 and 9 intermediate compression or pumping |
| 10 | riser (outside transportation scope) | 20 | intermediate compression or pumping |

Figure 1 — Schematic illustration of the system boundaries of this document

The boundary between transportation and storage/~~or~~ utilization is the point where the CO₂ stream leaves the transportation pipeline infrastructure and enters the downstream infrastructure, which can be permanent geological storage, utilization, or buffer storage prior to shipping.

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Carbon dioxide capture, transportation and geological storage — Pipeline transportation systems

1 Scope

This document specifies the requirements and recommendations for the transportation of CO₂ streams from the capture site to the storage facility where it is primarily stored in a geological formation or used for other purposes (e.g. for ~~EO~~enhanced oil recovery or CO₂ use).

This document applies to the transportation of CO₂ streams by:

- rigid metallic pipelines,
- pipeline systems,
- onshore and offshore pipelines for the transportation of CO₂ streams,
- conversion of existing pipelines for the transportation of CO₂ streams, and
- transportation of CO₂ streams in the gaseous and dense phases.

This document also includes aspects of CO₂ stream quality assurance, as well as converging CO₂ streams from different sources.

Health, safety and environment aspects specific to CO₂ transport and monitoring are also considered in this document.

Transportation of CO₂ via ship, rail or on road is not covered in this document.

2 Normative references

The following documents are referred to in the text in such a way that some or all of their content constitutes requirements of this document. For dated references, only the edition cited applies. For undated references, the latest edition of the referenced document (including any amendments) applies.

ISO 3183, *Petroleum and natural gas industries — Steel pipe for pipeline transportation systems*

ISO 20765-2, *Natural gas — Calculation of thermodynamic properties — Part 2: Single-phase properties (gas, liquid, and dense fluid) for extended ranges of application*

ISO/TR 27925, *Carbon dioxide capture, transportation, and geological storage — Cross cutting issues — Flow assurance*

API SPEC 5L, *Line Pipe, 46th Edition*

3 Terms and definitions

For the purposes of this document, the following terms and definitions apply.

ISO and IEC maintain terminology databases for use in standardization at the following addresses:

- —ISO Online browsing platform: available at <https://www.iso.org/obp>
- —IEC Electropedia: available at <https://www.electropedia.org/>

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3.1

aqueous phase

liquid phase composed predominantly of water and other impurities that are not dissolved in the gaseous or dense CO₂ phase

3.2

block valve

full-bore valve inserted into a pipeline to reduce the total volume of the CO₂ stream (3.4) that would be emitted in the case of planned or unplanned depressurization of that section or in the case of a pipeline rupture

3.3

bubble point pressure

pressure of the saturated liquid at a given composition and temperature (see ISO/TR 27925)

3.4

CO₂ stream

stream consisting overwhelmingly of carbon dioxide

Note 1 to entry: usually ≥ 95 mol% CO₂

3.5

corrosion allowance

additional wall thickness beyond that required by the mechanical design to compensate for any reduction in wall thickness by corrosion (internal/external) during the design operational life

3.6

critical point

highest temperature and pressure at which a pure substance (e.g. CO₂) can exist as a gas and a liquid in equilibrium

Note 1 to entry: For a multicomponent fluid mixture of a given composition, the critical point is the merge of the bubble point curve, and the dew point curve.

Note 2 to entry: The critical point is defined by the critical pressure (3.7) and critical temperature (3.8).

3.7

critical pressure

vapour pressure at the critical temperature (3.8)

Note 1 to entry: The critical pressure for pure CO₂ is 7,38 MPa.

3.8

critical temperature

for pure substance temperature above which liquid cannot be formed simply by increasing the pressure

Note 1 to entry: The critical temperature of pure CO₂ is 304,13 K (equivalent to 30,98 °C).

Note 2 to entry: For CO₂ streams (3.4), phase transitions can still occur above critical temperature.

3.9

dense phase

<engineering> CO₂ or CO₂ streams (3.4) in the single-phase fluid state above a density of 500 kg/m³

Note 1 to entry: For more details, see also ISO/TR 27925.