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Standard Test Method for Estimating Apparent Vapor Pressures and Molecular Weights of Lubricating Oils¹

This standard is issued under the fixed designation D2878; the number immediately following the designation indicates the year of original adoption or, in the case of revision, the year of last revision. A number in parentheses indicates the year of last reapproval. A superscript epsilon (ε) indicates an editorial change since the last revision or reapproval.

1. Scope

1.1 This test method covers a calculation procedure for converting data obtained by Test Method D972 to apparent vapor pressures and molecular weights. It has been demonstrated to be applicable to petroleum-based and synthetic ester lubricating oils, at temperatures of 395395 K to 535K (250535 K (250 °F) to 500 °F). However, its applicability to lubricating greases has not been established.

Note 1—Most lubricants boil over a fairly wide temperature range, a fact recognized in discussion of their vapor pressures. For example, the apparent vapor pressure over the range $\frac{90 \, \%}{2}$ to $0.1 \, \%$ evaporated may be as much as 100 times that over the range $\frac{4.94.9 \, \%}{2}$ to $5.0 \, \%$ evaporated.

- 1.2 The values stated in SI units are to be regarded as the standard. In cases in which materials, products, or equipment are available in inch-pound units only, SI units are omitted.
- 1.3 **WARNING**—Mercury has been designated by many regulatory agencies as a hazardous material that can cause central nervous system, kidney and liver damage. Mercury, or its vapor, may be hazardous to health and corrosive to materials. Caution should be taken when handling mercury and mercury containing products. See the applicable product Material Safety Data Sheet (MSDS) for details and EPA's website—http://www.epa.gov/mercury/faq.htm—for additional information. Users should be aware that selling mercury or mercury containing products into your state or country may be prohibited by law.
- 1.4 This standard does not purport to address all of the safety concerns, if any, associated with its use. It is the responsibility of the user of this standard to establish appropriate safety and health practices and determine the applicability or regulatory limitations prior to use. For specific warning statements, see 6.2, 7.1, 8.2, and Annex A2.

2. Referenced Documents

2.1 ASTM Standards:³

A240/A240M Specification for Chromium and Chromium-Nickel Stainless Steel Plate, Sheet, and Strip for Pressure Vessels and for General Applications and options and options and options and options are less than the control of the co

D92 Test Method for Flash and Fire Points by Cleveland Open Cup Tester

D972 Test Method for Evaporation Loss of Lubricating Greases and Oils

D2503 Test Method for Relative Molecular Mass (Molecular Weight) of Hydrocarbons by Thermoelectric Measurement of Vapor Pressure

D2595 Test Method for Evaporation Loss of Lubricating Greases Over Wide-Temperature Range

D2883 Test Method for Reaction Threshold Temperature of Liquid and Solid Materials

E659 Test Method for Autoignition Temperature of Chemicals

3. Terminology

- 3.1 Definitions of Terms Specific to This Standard:
- 3.1.1 apparent vapor pressure (p), n—the time-averaged value of the vapor pressure from the start to the end of the evaporation test.

¹ This test method is under the jurisdiction of Committee D02 on Petroleum Products, Liquid Fuels, and Lubricants and is the direct responsibility of Subcommittee D02.L0.07 on Engineering Sciences of High Performance Fluids and Solids (Formally D02.1100).

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² Coburn, J. F., "Lubricant Vapor Pressure Derived from Evaporation Loss," Transactions, American Society of Lubricating Engineers, ASLTA, Vol 12, 1969, pp. 129–134.

³ For referenced ASTM standards, visit the ASTM website, www.astm.org, or contact ASTM Customer Service at service@astm.org. For *Annual Book of ASTM Standards* volume information, refer to the standard's Document Summary page on the ASTM website.

3.1.1.1 Discussion—

While this may include some effects of differences in nonideality of the vapor, heat of vaporization, surface tension, and viscosity between the m-terphenyl and the lubricating oil, these factors have been demonstrated to be negligible. Unless stated, this average shall cover the range 0 to $5 \pm 1 \%$.

3.1.2 *cell constant (k), n*—the ratio of the amount of *m*-terphenyl or lubricating oil carried off per unit volume of gas to that predicted by Dalton's law.

$$k = 22.41 \ PW/VpM \tag{1}$$

where:

k = call constant

P = ambient atmospheric pressure, torr
W = mass of lubricant evaporated, g

V = volume of gas passed through all litres at 273K and 101.3 kPa (760 torr)

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p = apparent vapor pressure, torr

M = mole average molecular weight of lubricant vapor, g/mole

T = test temperature, K

It has been empirically determined that for *m*-terphenyl in air

$$k = 0.1266 - 12.60/(T - 273) \tag{2}$$

and that the cell constant is independent of the composition of the lubricant.

3.1.3 Test Method D972 is normally run with air, which may cause changes in easily oxidized fluids. In such cases, use of common reactive gas nitrogen and recalibration to obtain a slightly different cell constant (k') is mandatory.

4. Summary of Test Method

4.1 The test is run at the selected temperature for a sufficient time to give the selected amount of evaporation, which is 55 % $\pm 1 \%$ unless otherwise specified. This evaporation rate is compared with a standard value for pure *m*-terphenyl to yield the apparent vapor pressure and molecular weight of the lubricating oil as defined in Section 3.

5. Significance and Use

- 5.1 The vapor pressure of a substance as determined by measurement of evaporation reflects a property of the bulk sample. Little weight is given by the procedure to the presence of low concentrations of volatile impurities.
- 5.2 Vapor pressure, *per se*, is a thermodynamic property that is dependent only upon composition and temperature for stable systems. In the present method, composition changes occur during the course of the test so that the contribution of minor amounts of volatile impurities is minimized.

6. Apparatus

- 6.1 Evaporation Cell, as described in Annex A1.
- 6.2 Air Supply System, capable of supplying to the cell the required flow of air free of entrained particles (Warning—Compressed gas under high pressure. Use with extreme caution in the presence of combustible material, since the autoignition temperatures of most organic compounds in air are drastically reduced at elevated pressures. See Annex A2.1.). A 410-mm (16-in.) 410 mm (16 in.) length of 1-in.1 in. diameter pipe packed with glass wool has been found satisfactory for filtering the air.
 - 6.3 Oil Bath, as described in Annex A1.
- Note 2—Other constant-temperature baths may be used if the exit air passing over the grease sample is at the test temperature $(\pm 0.5K (1^{\circ}F))$. $(\pm 0.5 K (1^{\circ}F))$.
- 6.4 Temperature Measuring Devices—Resistance thermometers, thermocouples, or liquid-in-glass thermometers calibrated to accuracy within ± 0.5 °C (± 1.0 °F) ± 0.5 °C (± 1.0 °F) may be used. The use of mercury-in-glass thermometers of equal accuracy is permitted, although it is discouraged.

⁴ The sole source of supply of the apparatus known to the committee at this time is Flowrater meter, Fisher and Porter Co., Hatboro, PA. If you are aware of alternative suppliers, please provide this information to ASTM International Headquarters. Your comments will receive careful consideration at a meeting of the responsible technical committee, ¹ which you may attend.

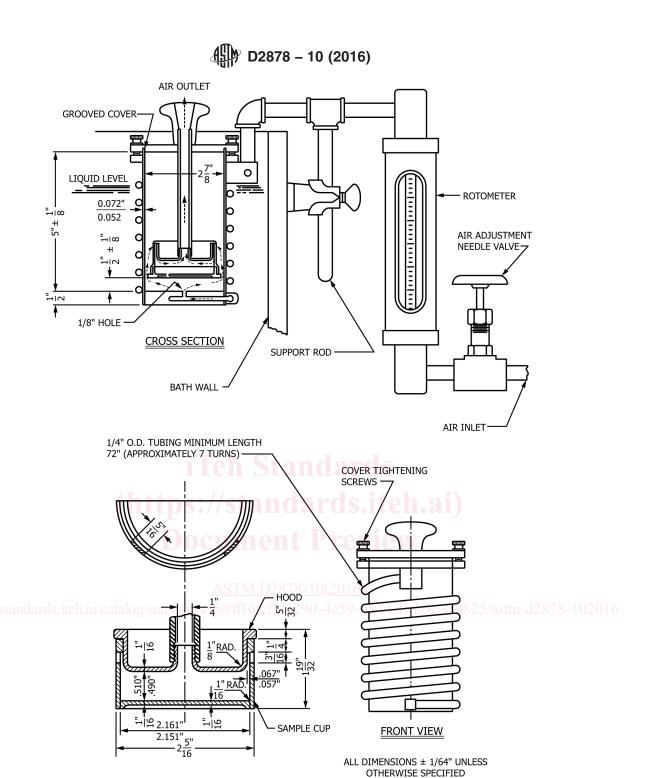


FIG. 1 Evaporation Test Cell

6.6 Oil Sample Cup, as described in Fig. 1 and A1.1.2.

7. Calibration of Equipment

7.1 It is assumed that equipment conforming to Test Method D972 in design and installation needs no calibration. If questions arise, carry out the procedure using *m*-terphenyl (**Warning**—Harmful or fatal if swallowed. See A2.2.) of good commercial quality. The following two points shall be determined:

	Temperature		Evaporation to Conform
K	°F	Time, h	to Eq 2, g
395	250	22	0.267 ± 0.027
420	300	6.5	0.503 ± 0.050