



Designation: **D1555–09 D1555–16**

Standard Test Method for Calculation of Volume and Weight of Industrial Aromatic Hydrocarbons and Cyclohexane¹

This standard is issued under the fixed designation D1555; the number immediately following the designation indicates the year of original adoption or, in the case of revision, the year of last revision. A number in parentheses indicates the year of last reapproval. A superscript epsilon (ϵ) indicates an editorial change since the last revision or reapproval.

This standard has been approved for use by agencies of the U.S. Department of Defense.

1. Scope*

1.1 This standard is for use in calculating the weight and volume of benzene, toluene, mixed xylenes, styrene, ortho-xylene, meta-xylene, para-xylene, cumene, ethylbenzene, 300 to 350°F and 350 to 400°F aromatic hydrocarbons, and cyclohexane. A method is given for calculating the volume at 60°F from an observed volume at $t^\circ\text{F}$. **Table 1** lists the density *in pounds vacuo per gallon* at 60°F for high purity chemicals; chemicals used to develop the relationship. Densities (or weights) “in vacuo” represent the true density (or weight) if measured in a vacuum without the buoyancy effect of air acting on the liquid. It is representative of the actual amount of product present. Densities (or weights) “in air” represent what would actually be measured on a scale. The difference is on the order of 0.13 %. Modern densitometers measure density in vacuo and the ASTM recommends the use of in vacuo densities (or weights).

~~1.2 Calculated results shall be rounded off in accordance with the rounding-off method of Practice E29.~~

1.2 The values stated in inch-pound units are to be regarded as standard. No other units of measurement are included in this standard.

1.2.1 A complete SI unit companion standard has been developed in Test Method **D1555M**.

1.3 *This standard does not purport to address all of the safety concerns, if any, associated with its use. It is the responsibility of the user of this standard to establish appropriate safety and health practices and determine the applicability of regulatory limitations prior to use.*

2. Referenced Documents

2.1 *ASTM Standards:*²

D1217 Test Method for Density and Relative Density (Specific Gravity) of Liquids by Bingham Pycnometer

D1555M Test Method for Calculation of Volume and Weight of Industrial Aromatic Hydrocarbons and Cyclohexane [Metric]

D3505 Test Method for Density or Relative Density of Pure Liquid Chemicals

D4052 Test Method for Density, Relative Density, and API Gravity of Liquids by Digital Density Meter

~~**E29** Practice for Using Significant Digits in Test Data to Determine Conformance with Specifications~~

2.2 *Other Documents:*

American Petroleum Society Research Project 44³

Patterson, J. B., and Morris, E. C. *Metrologia*, 31, 1994, pp. 277-288

NSRDS-NIST 75-121 TRC Thermodynamic Tables—Hydrocarbons, Supplement No. 121, April 30, 2001⁴

3. Significance and Use

3.1 This test method is suitable for use in calculating weights and volumes of the products outlined in Section 1. The information presented in this method can be used for determining quantities of the above-stated aromatic hydrocarbons in tanks, shipping containers, etc.

¹ This test method is under the jurisdiction of ASTM Committee **D16** on Aromatic Hydrocarbons and Related Chemicals and is the direct responsibility of Subcommittee **D16.01** on Benzene, Toluene, Xylenes, Cyclohexane and Their Derivatives.

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² For referenced ASTM standards, visit the ASTM website, www.astm.org, or contact ASTM Customer Service at service@astm.org. For *Annual Book of ASTM Standards* volume information, refer to the ~~standard's~~ standard's Document Summary page on the ASTM website.

³ “Selected Values of Properties of Hydrocarbons and Related Compounds,” prepared by American Petroleum Institute Research Project 44 at the Chemical Thermodynamics Center, Department of Chemistry, Texas A&M, College Station, TX.

⁴ Available from National Institute of Standards and Technology (NIST), 100 Bureau Dr., Stop 1070, Gaithersburg, MD 20899-1070, http://www.nist.gov.

*A Summary of Changes section appears at the end of this standard

TABLE 1 Physical Properties

| Product | Freezing Point °F | Boiling Point °F | 60°F-Density <i>in Vacuo</i> at 60°F g/cc ^{A,B} | Density <i>in Vacuo</i> at 60°F lb/gal ^C | Density <i>in Air</i> at 60°F lb/gal ^D |
|------------------|-------------------|------------------|--|---|---|
| Benzene | 42.0 | 176.2 | 0.88373 | 7.3751 | 7.3662 |
| Cumene | -140.9 | 306.3 | 0.86538 | 7.2219 | 7.2130 |
| Cyclohexane | 43.8 | 177.3 | 0.78265 | 6.5315 | 6.5225 |
| Ethylbenzene | -139.0 | 277.1 | 0.87077 | 7.2669 | 7.2580 |
| Styrene | -23.1 | 293.4 | 0.90979 | 7.5926 | 7.5837 |
| Toluene | -139.0 | 231.1 | 0.87096 | 7.2685 | 7.2596 |
| <i>m</i> -Xylene | -54.2 | 282.4 | 0.86784 | 7.2425 | 7.2336 |
| <i>o</i> -Xylene | -13.3 | 291.9 | 0.88340 | 7.3723 | 7.3634 |
| <i>p</i> -Xylene | 55.9 | 281.0 | 0.86456 | 7.2151 | 7.2062 |

^A Based on regression of 2001 TRC Thermodynamic Tables, Hydrocarbons, NSRDS-NIST 75-121 (April 30, 2001). The data is presented in [Appendix X1](#).

^B Specific Gravity has been deleted from this table as unnecessary to this standard. If needed, divide 60°F density in g/cc divided by 0.999016 g/cc. See [Appendix X2](#).

^C Produced by multiplying the density *in vacuo* at 60°F in g/cc by 8.345404388.345404452 and rounding to 4 decimal places.

^D Produced using $\text{lb/gal} = (\text{Density} - \text{g/cc in air} \cdot 1.000149925971.000149926 - 0.00119940779543) \cdot 8.345404388.345404452$, rounding to 4 decimal places. See [Appendix X3](#).

NOTE 1—Densities (or weights) “*in vacuo*” represent the true density (or weight) if measured in a vacuum without the buoyancy effect of air acting on the liquid. It is representative of the actual amount of product present. Densities (or weights) “*in air*” represent what would actually be measured on a scale. The difference is on the order of 0.13 %. Modern densitometers measure density *in vacuo* and the ASTM and API recommend the use of *in vacuo* densities (or weights); however, the purchaser and seller should agree on which to use in their transactions.

4. Basic Data

4.1 Densities of materials should be determined by measurement (see [Section 7](#)). Densities of pure materials at 60°F are derived may be estimated from densities furnished by NSRDS-NIST 75-121 (National Standard Reference Data Series—National Institute of Standards and Technology). Densities of impure materials should be determined by actual measurement (see [Section 7](#)).

4.2 The VCF (Volume Correction Factor) equations provided below were derived from the Volume Correction Tables presented in the previous edition of this standard, Method D1555-95. Although reported as based on the American Petroleum Institute Research Project 44, the actual documentation that could be found is incomplete. As regression of the NIST data ([Appendix X1](#)) provided VCFs that differ from the historical VCFs by only 0 to ± 0.12 % (depending on the compound), the decision was made to use the previous method’s VCF tables.

4.3 The VCF tables were regressed with a commercially available data regression program (TableCurve 2D V4). However, any modern regression program should produce the same results.

4.4 The former VCF tables were based on data for compounds of the highest purity, used in American Petroleum Institute Research Project 44 for which the purity is not clearly defined, but were reported to be usable for materials in the ranges indicated in [Table 2](#). The data supporting this conclusion appears to be unavailable at the present time; however there is no reason to change this recommendation. If, depending on the composition of the impurities, there is reason to suspect that the VCF implementation procedures presented below do not apply to a particular impure product, a separate implementation procedure should be independently determined. This may be done by measuring the density of a representative sample at different temperatures throughout the expected working temperature range, regressing the data to obtain a temperature/density equation that best reproduces the observed data, and then dividing the constants of the temperature/density equation by the calculated density at 60°F. Alternatively, if the composition has been quantified one can use the VCFs of each component (if available) to calculate a weighted average density at different temperatures and then process the data as mentioned above.

TABLE 2 Application Range of Implementation Procedure

| Impure Products | Range |
|---------------------------------|-----------------|
| Benzene | 95 to 100% |
| Cumene | 95 to 100% |
| Cyclohexane | 90 to 100% |
| Ethylbenzene | 95 to 100% |
| Styrene | 95 to 100% |
| Toluene | 95 to 100% |
| Mixed Xylenes | All proportions |
| <i>m</i> -Xylene | 95 to 100% |
| <i>o</i> -Xylene | 95 to 100% |
| <i>p</i> -Xylene | 94 to 100% |
| 300-350°F Aromatic Hydrocarbons | All proportions |
| 350-400°F Aromatic Hydrocarbons | All proportions |

5. Volume Correction Factor Implementation Procedure

5.1 The following general equation is used to generate the Volume Correction Factors:

$$VCF = a + bt + ct^2 + dt^3 + et^4 \quad (1)$$

$$VCF = a + bt + ct^2 + dt^3 + et^4 \quad (1)$$

where:

t = temperature in °F

where:

t = temperature in °F

and constants a through e are specific to each compound (presented in [Table 3](#)).

5.1.1 Temperature may be entered in tenths of a degree Fahrenheit.

5.1.2 The final calculated result is rounded to 5 places past the decimal, the appropriate significant figures if it is to be reported and not rounded if to be used in another calculation. No intermediate rounding or truncation should be done.

5.1.3 The equations are valid for liquid product up to 140°F (150°F for *p*-xylene).

5.1.4 This implementation procedure replaces the printed tables of the table in a previous edition of this Method standard (Method D1555-95) for determining VCFs. **The implementation procedure is the Standard, not the printed tables, table.** However, a printout of the implementation procedure the printed table is provided in 1°F increments for the user's user's convenience ([Table 4](#)).

6. Use of the Implementation Procedure

6.1 *Convert Volume Reduction to 60°F*—Enter the appropriate equation with the temperature to the nearest 0.1 degree Fahrenheit at which the bulk volume was measured (temperature t). After performing the mathematical operations, round the resulting VCF to 5 places past the decimal. Multiply the bulk volume measurement at temperature t by the VCF.

Note 1—The purchaser and seller should agree on a reasonable policy in regard to rounding of final numbers in all computations. Rounding the final weight or volume to five significant figures is, in most cases, also acceptable.

6.1.1 *Example 1*—What is the volume at 60°F of a tank car of *p*-xylene whose volume was measured to be 9280 gal at a mean temperature of 88.7°F?

6.1.1.1 Enter [Eq 1](#) with 88.7 88.7°F and the appropriate constants from [Table 3](#) into [Eq 1](#) to calculate a VCF of 0.98414. The 0.984143256178277. Multiply the volume at 60°F is: 88.7°F by the VCF to obtain the volume at 60°F.

$$9280 \times 0.98414 = 9132.8 \text{ gal}$$

$$9280 \text{ gal} \times 0.984143256178277 = 9,132.84941733442 \text{ or } 9133 \text{ gal}$$

If this value is to be reported, it may be rounded as required by the user. The unrounded intermediate value should be used for additional calculations.

6.2 *Converting Volume to Weight for Chemicals Listed in Table 1*—Multiply the volume in gallons at 60°F (5 digits) by the appropriate density in pounds per gallon at 60°F (see [Table 1](#) and [Table 1 Note](#)):

6.2.1 *Example 2*—What is the weight of *p*-xylene whose net volume is 9132.8 gal?

6.2.1.1 The weight is:

$$9132.8 \times 7.2151 = 65,894 \text{ lb in vacuo}$$

or

$$9132.8 \times 7.2062 = 65,813 \text{ lb in air}$$

TABLE 3 VCF Constants

| Product | a | b | c | d | eE |
|-------------------------------|-------------|--------------------------|---------------------------|----------------------------|---------------------------|
| Benzene | 1.038382492 | -6.2307×10^{-4} | -2.8505×10^{-7} | 1.2692×10^{-10} | 0 |
| Cumene | 1.032401114 | -5.3445×10^{-4} | -9.5067×10^{-8} | 3.6272×10^{-11} | 0 |
| Cyclohexane | 1.039337296 | -6.4728×10^{-4} | -1.4582×10^{-7} | 1.03538×10^{-10} | 0 |
| Ethylbenzene | 1.033346632 | -5.5243×10^{-4} | 8.37035×10^{-10} | -1.2692×10^{-9} | 5.55061×10^{-12} |
| Styrene | 1.032227515 | -5.3444×10^{-4} | -4.4323×10^{-8} | 0 | 0 |
| Toluene | 1.035323647 | -5.8887×10^{-4} | 2.46508×10^{-9} | -7.2802×10^{-12} | 0 |
| <i>m</i> -Xylene ^A | 1.031887514 | -5.2326×10^{-4} | -1.3253×10^{-7} | -7.35960×10^{-11} | 0 |
| <i>o</i> -Xylene | 1.031436449 | -5.2302×10^{-4} | -2.5217×10^{-9} | -2.13840×10^{-10} | 0 |
| <i>p</i> -Xylene | 1.032307000 | -5.2815×10^{-4} | -1.8416×10^{-7} | 1.89256×10^{-10} | 0 |
| 300-350°F | 1.031118000 | -5.1827×10^{-4} | -3.5109×10^{-9} | -1.98360×10^{-11} | 0 |
| 350-400°F | 1.029099000 | -4.8287×10^{-4} | -3.7692×10^{-8} | 3.78575×10^{-11} | 0 |

^Aand Mixed Xylenes.

TABLE 4 Volume Correction Factors

Volume Correction to 60°F

| Temperature °F | Benzene | Cumene | Cyclohexane | Ethylbenzene | Styrene | Toluene | <i>m</i> -Xylene and Mixed Xylenes | <i>o</i> -Xylene | <i>p</i> -Xylene | 300 to 350° Aromatic Hydrocarbons | 350 to 400° Aromatic Hydrocarbons |
|-------------------|---------|---------|-------------|--------------|---------|---------|---|------------------|------------------|---|---|
| -5.0 | ... | ... | ... | ... | ... | 1.03827 | ... | ... | ... | ... | ... |
| -4.0 | ... | ... | ... | ... | ... | 1.03768 | ... | ... | ... | ... | ... |
| -3.0 | ... | ... | ... | ... | ... | 1.03709 | ... | ... | ... | ... | ... |
| -2.0 | ... | ... | ... | ... | ... | 1.03650 | ... | ... | ... | ... | ... |
| -1.0 | ... | ... | ... | ... | ... | 1.03591 | ... | ... | ... | ... | ... |
| 0.0 | ... | ... | ... | ... | ... | 1.03532 | ... | ... | ... | ... | ... |
| 1.0 | ... | ... | ... | ... | ... | 1.03473 | ... | ... | ... | ... | ... |
| 2.0 | ... | ... | ... | ... | ... | 1.03415 | ... | ... | ... | ... | ... |
| 3.0 | ... | ... | ... | ... | ... | 1.03356 | ... | ... | ... | ... | ... |
| 4.0 | ... | ... | ... | ... | ... | 1.03297 | ... | ... | ... | ... | ... |
| 5.0 | ... | 1.02973 | ... | 1.03058 | ... | 1.03238 | 1.02927 | 1.02882 | ... | 1.02853 | 1.02668 |
| 6.0 | ... | 1.02919 | ... | 1.03003 | ... | 1.03179 | 1.02874 | 1.02830 | ... | 1.02801 | 1.02620 |
| 7.0 | ... | 1.02866 | ... | 1.02948 | ... | 1.03120 | 1.02822 | 1.02778 | ... | 1.02749 | 1.02572 |
| 8.0 | ... | 1.02812 | ... | 1.02893 | ... | 1.03061 | 1.02769 | 1.02725 | ... | 1.02697 | 1.02523 |
| 9.0 | ... | 1.02758 | ... | 1.02837 | ... | 1.03002 | 1.02717 | 1.02673 | ... | 1.02645 | 1.02475 |
| 10.0 | ... | 1.02705 | ... | 1.02782 | ... | 1.02944 | 1.02664 | 1.02621 | ... | 1.02593 | 1.02427 |
| 11.0 | ... | 1.02651 | ... | 1.02727 | ... | 1.02885 | 1.02612 | 1.02568 | ... | 1.02542 | 1.02378 |
| 12.0 | ... | 1.02597 | ... | 1.02672 | ... | 1.02826 | 1.02559 | 1.02516 | ... | 1.02490 | 1.02330 |
| 13.0 | ... | 1.02544 | ... | 1.02616 | ... | 1.02767 | 1.02506 | 1.02464 | ... | 1.02438 | 1.02282 |
| 14.0 | ... | 1.02490 | ... | 1.02561 | ... | 1.02708 | 1.02454 | 1.02411 | ... | 1.02386 | 1.02233 |
| 15.0 | ... | 1.02436 | ... | 1.02506 | 1.02420 | 1.02649 | 1.02401 | 1.02359 | ... | 1.02334 | 1.02185 |
| 16.0 | ... | 1.02383 | ... | 1.02450 | 1.02367 | 1.02590 | 1.02348 | 1.02307 | ... | 1.02282 | 1.02136 |
| 17.0 | ... | 1.02329 | ... | 1.02395 | 1.02313 | 1.02531 | 1.02295 | 1.02254 | ... | 1.02231 | 1.02088 |
| 18.0 | ... | 1.02275 | ... | 1.02340 | 1.02259 | 1.02472 | 1.02243 | 1.02202 | ... | 1.02179 | 1.02040 |
| 19.0 | ... | 1.02221 | ... | 1.02284 | 1.02206 | 1.02414 | 1.02190 | 1.02150 | ... | 1.02127 | 1.01991 |
| 20.0 | ... | 1.02167 | ... | 1.02229 | 1.02152 | 1.02355 | 1.02137 | 1.02097 | ... | 1.02075 | 1.01943 |
| 21.0 | ... | 1.02114 | ... | 1.02174 | 1.02098 | 1.02296 | 1.02084 | 1.02045 | ... | 1.02023 | 1.01894 |
| 22.0 | ... | 1.02060 | ... | 1.02118 | 1.02045 | 1.02237 | 1.02031 | 1.01993 | ... | 1.01971 | 1.01846 |
| 23.0 | ... | 1.02006 | ... | 1.02063 | 1.01991 | 1.02178 | 1.01978 | 1.01940 | ... | 1.01920 | 1.01797 |
| 24.0 | ... | 1.01952 | ... | 1.02007 | 1.01938 | 1.02119 | 1.01925 | 1.01888 | ... | 1.01868 | 1.01749 |
| 25.0 | ... | 1.01898 | ... | 1.01952 | 1.01884 | 1.02060 | 1.01872 | 1.01836 | ... | 1.01816 | 1.01700 |
| 26.0 | ... | 1.01844 | ... | 1.01896 | 1.01830 | 1.02001 | 1.01819 | 1.01783 | ... | 1.01764 | 1.01652 |
| 27.0 | ... | 1.01790 | ... | 1.01841 | 1.01777 | 1.01943 | 1.01766 | 1.01731 | ... | 1.01712 | 1.01603 |
| 28.0 | ... | 1.01736 | ... | 1.01785 | 1.01723 | 1.01884 | 1.01713 | 1.01679 | ... | 1.01660 | 1.01555 |
| 29.0 | ... | 1.01682 | ... | 1.01730 | 1.01669 | 1.01825 | 1.01660 | 1.01626 | ... | 1.01608 | 1.01506 |
| 30.0 | ... | 1.01628 | ... | 1.01674 | 1.01615 | 1.01766 | 1.01607 | 1.01574 | ... | 1.01557 | 1.01458 |
| 31.0 | ... | 1.01574 | ... | 1.01619 | 1.01562 | 1.01707 | 1.01554 | 1.01521 | ... | 1.01505 | 1.01409 |
| 32.0 | ... | 1.01520 | ... | 1.01563 | 1.01508 | 1.01648 | 1.01501 | 1.01469 | ... | 1.01453 | 1.01361 |
| 33.0 | ... | 1.01466 | ... | 1.01508 | 1.01454 | 1.01589 | 1.01447 | 1.01417 | ... | 1.01401 | 1.01312 |
| 34.0 | ... | 1.01412 | ... | 1.01452 | 1.01401 | 1.01530 | 1.01394 | 1.01364 | ... | 1.01349 | 1.01264 |
| 35.0 | ... | 1.01358 | ... | 1.01397 | 1.01347 | 1.01472 | 1.01341 | 1.01312 | ... | 1.01297 | 1.01215 |
| 36.0 | ... | 1.01304 | ... | 1.01341 | 1.01293 | 1.01413 | 1.01287 | 1.01259 | ... | 1.01245 | 1.01167 |
| 37.0 | ... | 1.01250 | ... | 1.01285 | 1.01239 | 1.01354 | 1.01234 | 1.01207 | ... | 1.01194 | 1.01118 |
| 38.0 | ... | 1.01196 | ... | 1.01230 | 1.01185 | 1.01295 | 1.01181 | 1.01155 | ... | 1.01142 | 1.01070 |
| 39.0 | ... | 1.01142 | ... | 1.01174 | 1.01132 | 1.01236 | 1.01127 | 1.01102 | ... | 1.01090 | 1.01021 |
| 40.0 | ... | 1.01087 | ... | 1.01118 | 1.01078 | 1.01177 | 1.01074 | 1.01050 | ... | 1.01038 | 1.00973 |
| 41.0 | ... | 1.01033 | ... | 1.01063 | 1.01024 | 1.01118 | 1.01021 | 1.00997 | ... | 1.00986 | 1.00924 |
| 42.0 | ... | 1.00979 | ... | 1.01007 | 1.00970 | 1.01059 | 1.00967 | 1.00945 | ... | 1.00934 | 1.00875 |
| 43.0 | 1.01107 | 1.00925 | ... | 1.00951 | 1.00916 | 1.01001 | 1.00914 | 1.00892 | ... | 1.00882 | 1.00827 |
| 44.0 | 1.01043 | 1.00870 | 1.01058 | 1.00895 | 1.00863 | 1.00942 | 1.00860 | 1.00840 | ... | 1.00831 | 1.00778 |
| 45.0 | 1.00978 | 1.00816 | 1.00992 | 1.00840 | 1.00809 | 1.00883 | 1.00807 | 1.00788 | ... | 1.00779 | 1.00730 |
| 46.0 | 1.00913 | 1.00762 | 1.00926 | 1.00784 | 1.00755 | 1.00824 | 1.00753 | 1.00735 | ... | 1.00727 | 1.00681 |
| 47.0 | 1.00848 | 1.00708 | 1.00860 | 1.00728 | 1.00701 | 1.00765 | 1.00699 | 1.00683 | ... | 1.00675 | 1.00632 |
| 48.0 | 1.00783 | 1.00653 | 1.00794 | 1.00672 | 1.00647 | 1.00706 | 1.00646 | 1.00630 | ... | 1.00623 | 1.00584 |
| 49.0 | 1.00718 | 1.00599 | 1.00728 | 1.00616 | 1.00593 | 1.00647 | 1.00592 | 1.00578 | ... | 1.00571 | 1.00535 |
| 50.0 | 1.00653 | 1.00545 | 1.00662 | 1.00560 | 1.00539 | 1.00589 | 1.00538 | 1.00525 | ... | 1.00519 | 1.00487 |
| 51.0 | 1.00588 | 1.00490 | 1.00596 | 1.00504 | 1.00486 | 1.00530 | 1.00485 | 1.00473 | ... | 1.00467 | 1.00438 |
| 52.0 | 1.00523 | 1.00436 | 1.00530 | 1.00448 | 1.00432 | 1.00471 | 1.00431 | 1.00420 | ... | 1.00416 | 1.00389 |
| 53.0 | 1.00458 | 1.00381 | 1.00464 | 1.00393 | 1.00378 | 1.00412 | 1.00377 | 1.00368 | ... | 1.00364 | 1.00341 |
| 54.0 | 1.00393 | 1.00327 | 1.00398 | 1.00337 | 1.00324 | 1.00353 | 1.00323 | 1.00315 | ... | 1.00312 | 1.00292 |
| 55.0 | 1.00327 | 1.00272 | 1.00331 | 1.00281 | 1.00270 | 1.00294 | 1.00270 | 1.00263 | ... | 1.00260 | 1.00243 |
| 56.0 | 1.00262 | 1.00218 | 1.00265 | 1.00224 | 1.00216 | 1.00235 | 1.00216 | 1.00210 | 1.00219 | 1.00208 | 1.00195 |
| 57.0 | 1.00196 | 1.00164 | 1.00199 | 1.00168 | 1.00162 | 1.00176 | 1.00162 | 1.00158 | 1.00164 | 1.00156 | 1.00146 |
| 58.0 | 1.00131 | 1.00109 | 1.00132 | 1.00112 | 1.00108 | 1.00118 | 1.00108 | 1.00105 | 1.00109 | 1.00104 | 1.00097 |
| 59.0 | 1.00066 | 1.00055 | 1.00066 | 1.00056 | 1.00054 | 1.00059 | 1.00054 | 1.00053 | 1.00054 | 1.00052 | 1.00049 |
| 60.0 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 | 1.00000 |
| 61.0 | 0.99934 | 0.99945 | 0.99933 | 0.99944 | 0.99946 | 0.99941 | 0.99946 | 0.99947 | 0.99945 | 0.99949 | 0.99951 |
| 62.0 | 0.99869 | 0.99891 | 0.99867 | 0.99888 | 0.99892 | 0.99882 | 0.99892 | 0.99895 | 0.99890 | 0.99897 | 0.99903 |
| 63.0 | 0.99803 | 0.99836 | 0.99801 | 0.99832 | 0.99838 | 0.99823 | 0.99838 | 0.99842 | 0.99835 | 0.99845 | 0.99854 |
| 64.0 | 0.99737 | 0.99782 | 0.99734 | 0.99775 | 0.99784 | 0.99764 | 0.99784 | 0.99790 | 0.99780 | 0.99793 | 0.99805 |
| 65.0 | 0.99671 | 0.99727 | 0.99668 | 0.99719 | 0.99730 | 0.99706 | 0.99730 | 0.99737 | 0.99725 | 0.99741 | 0.99756 |

TABLE 4 *Continued*

Volume Correction to 60°F

| Temperature °F | Benzene | Cumene | Cyclohexane | Ethylbenzene | Styrene | Toluene | <i>m</i> -Xylene and Mixed Xylenes | <i>o</i> -Xylene | <i>p</i> -Xylene | 300 to 350° Aromatic Hydrocarbons | 350 to 400° Aromatic Hydrocarbons |
|-------------------|---------|---------|-------------|--------------|---------|---------|---|------------------|------------------|---|---|
| 66.0 | 0.99605 | 0.99672 | 0.99601 | 0.99663 | 0.99676 | 0.99647 | 0.99675 | 0.99684 | 0.99670 | 0.99689 | 0.99708 |
| 67.0 | 0.99540 | 0.99618 | 0.99535 | 0.99607 | 0.99622 | 0.99588 | 0.99621 | 0.99632 | 0.99615 | 0.99637 | 0.99659 |
| 68.0 | 0.99474 | 0.99563 | 0.99468 | 0.99550 | 0.99568 | 0.99529 | 0.99567 | 0.99579 | 0.99560 | 0.99585 | 0.99610 |
| 69.0 | 0.99408 | 0.99508 | 0.99401 | 0.99494 | 0.99514 | 0.99470 | 0.99513 | 0.99527 | 0.99505 | 0.99533 | 0.99561 |
| 70.0 | 0.99341 | 0.99454 | 0.99335 | 0.99438 | 0.99460 | 0.99411 | 0.99458 | 0.99474 | 0.99450 | 0.99482 | 0.99513 |
| 71.0 | 0.99275 | 0.99399 | 0.99268 | 0.99382 | 0.99406 | 0.99352 | 0.99404 | 0.99421 | 0.99395 | 0.99430 | 0.99464 |
| 72.0 | 0.99209 | 0.99344 | 0.99202 | 0.99325 | 0.99352 | 0.99294 | 0.99350 | 0.99369 | 0.99340 | 0.99378 | 0.99415 |
| 73.0 | 0.99143 | 0.99289 | 0.99135 | 0.99269 | 0.99298 | 0.99235 | 0.99295 | 0.99316 | 0.99284 | 0.99326 | 0.99366 |
| 74.0 | 0.99077 | 0.99235 | 0.99068 | 0.99212 | 0.99244 | 0.99176 | 0.99241 | 0.99263 | 0.99229 | 0.99274 | 0.99318 |
| 75.0 | 0.99010 | 0.99180 | 0.99001 | 0.99156 | 0.99190 | 0.99117 | 0.99187 | 0.99211 | 0.99174 | 0.99222 | 0.99269 |
| 76.0 | 0.98944 | 0.99125 | 0.98935 | 0.99099 | 0.99135 | 0.99058 | 0.99132 | 0.99158 | 0.99119 | 0.99170 | 0.99220 |
| 77.0 | 0.98877 | 0.99070 | 0.98868 | 0.99043 | 0.99081 | 0.98999 | 0.99078 | 0.99105 | 0.99063 | 0.99118 | 0.99171 |
| 78.0 | 0.98811 | 0.99015 | 0.98801 | 0.98987 | 0.99027 | 0.98940 | 0.99023 | 0.99052 | 0.99008 | 0.99066 | 0.99122 |
| 79.0 | 0.98744 | 0.98960 | 0.98734 | 0.98930 | 0.98973 | 0.98881 | 0.98969 | 0.98981 | 0.98953 | 0.99014 | 0.99074 |
| 80.0 | 0.98678 | 0.98906 | 0.98667 | 0.98874 | 0.98919 | 0.98823 | 0.98914 | 0.98947 | 0.98897 | 0.98962 | 0.99025 |
| 81.0 | 0.98611 | 0.98851 | 0.98601 | 0.98817 | 0.98865 | 0.98764 | 0.98859 | 0.98894 | 0.98842 | 0.98910 | 0.98976 |
| 82.0 | 0.98544 | 0.98796 | 0.98534 | 0.98760 | 0.98811 | 0.98705 | 0.98805 | 0.98841 | 0.98786 | 0.98859 | 0.98927 |
| 83.0 | 0.98478 | 0.98741 | 0.98467 | 0.98704 | 0.98756 | 0.98646 | 0.98750 | 0.98789 | 0.98731 | 0.98807 | 0.98878 |
| 84.0 | 0.98411 | 0.98686 | 0.98400 | 0.98647 | 0.98702 | 0.98587 | 0.98695 | 0.98736 | 0.98676 | 0.98755 | 0.98829 |
| 85.0 | 0.98344 | 0.98631 | 0.98333 | 0.98591 | 0.98648 | 0.98528 | 0.98641 | 0.98683 | 0.98620 | 0.98703 | 0.98781 |
| 86.0 | 0.98277 | 0.98576 | 0.98266 | 0.98534 | 0.98594 | 0.98469 | 0.98586 | 0.98630 | 0.98564 | 0.98651 | 0.98732 |
| 87.0 | 0.98210 | 0.98521 | 0.98199 | 0.98477 | 0.98540 | 0.98411 | 0.98531 | 0.98577 | 0.98509 | 0.98599 | 0.98683 |
| 88.0 | 0.98143 | 0.98466 | 0.98132 | 0.98421 | 0.98485 | 0.98352 | 0.98476 | 0.98525 | 0.98453 | 0.98547 | 0.98634 |
| 89.0 | 0.98076 | 0.98411 | 0.98065 | 0.98364 | 0.98431 | 0.98293 | 0.98422 | 0.98472 | 0.98398 | 0.98495 | 0.98585 |
| 90.0 | 0.98009 | 0.98356 | 0.97998 | 0.98307 | 0.98377 | 0.98234 | 0.98367 | 0.98419 | 0.98342 | 0.98443 | 0.98536 |
| 91.0 | 0.97942 | 0.98301 | 0.97931 | 0.98251 | 0.98323 | 0.98175 | 0.98312 | 0.98366 | 0.98286 | 0.98391 | 0.98487 |
| 92.0 | 0.97875 | 0.98246 | 0.97863 | 0.98194 | 0.98268 | 0.98116 | 0.98257 | 0.98313 | 0.98231 | 0.98339 | 0.98439 |
| 93.0 | 0.97807 | 0.98190 | 0.97796 | 0.98137 | 0.98214 | 0.98057 | 0.98202 | 0.98260 | 0.98175 | 0.98287 | 0.98390 |
| 94.0 | 0.97740 | 0.98135 | 0.97729 | 0.98080 | 0.98160 | 0.97999 | 0.98147 | 0.98207 | 0.98119 | 0.98235 | 0.98341 |
| 95.0 | 0.97673 | 0.98080 | 0.97662 | 0.98024 | 0.98106 | 0.97940 | 0.98092 | 0.98154 | 0.98063 | 0.98183 | 0.98292 |
| 96.0 | 0.97605 | 0.98025 | 0.97595 | 0.97967 | 0.98051 | 0.97881 | 0.98037 | 0.98101 | 0.98007 | 0.98131 | 0.98243 |
| 97.0 | 0.97538 | 0.97970 | 0.97527 | 0.97910 | 0.97997 | 0.97822 | 0.97982 | 0.98048 | 0.97952 | 0.98079 | 0.98194 |
| 98.0 | 0.97470 | 0.97915 | 0.97460 | 0.97853 | 0.97943 | 0.97763 | 0.97927 | 0.97996 | 0.97896 | 0.98028 | 0.98145 |
| 99.0 | 0.97403 | 0.97859 | 0.97393 | 0.97797 | 0.97888 | 0.97704 | 0.97871 | 0.97943 | 0.97840 | 0.97976 | 0.98096 |
| 100.0 | 0.97335 | 0.97804 | 0.97325 | 0.97740 | 0.97834 | 0.97645 | 0.97816 | 0.97890 | 0.97784 | 0.97924 | 0.98047 |
| 101.0 | 0.97268 | 0.97749 | 0.97258 | 0.97683 | 0.97780 | 0.97587 | 0.97761 | 0.97837 | 0.97728 | 0.97872 | 0.97998 |
| 102.0 | 0.97200 | 0.97694 | 0.97191 | 0.97626 | 0.97725 | 0.97528 | 0.97706 | 0.97784 | 0.97672 | 0.97820 | 0.97949 |
| 103.0 | 0.97132 | 0.97638 | 0.97123 | 0.97569 | 0.97671 | 0.97469 | 0.97651 | 0.97730 | 0.97616 | 0.97768 | 0.97900 |
| 104.0 | 0.97064 | 0.97583 | 0.97056 | 0.97512 | 0.97617 | 0.97410 | 0.97595 | 0.97677 | 0.97560 | 0.97716 | 0.97852 |
| 105.0 | 0.96996 | 0.97528 | 0.96989 | 0.97456 | 0.97562 | 0.97351 | 0.97540 | 0.97624 | 0.97504 | 0.97664 | 0.97803 |
| 106.0 | 0.96929 | 0.97472 | 0.96921 | 0.97399 | 0.97508 | 0.97292 | 0.97485 | 0.97571 | 0.97448 | 0.97612 | 0.97754 |
| 107.0 | 0.96861 | 0.97417 | 0.96854 | 0.97342 | 0.97453 | 0.97233 | 0.97429 | 0.97518 | 0.97392 | 0.97560 | 0.97705 |
| 108.0 | 0.96793 | 0.97362 | 0.96786 | 0.97285 | 0.97399 | 0.97175 | 0.97374 | 0.97465 | 0.97336 | 0.97508 | 0.97656 |
| 109.0 | 0.96725 | 0.97306 | 0.96719 | 0.97228 | 0.97345 | 0.97116 | 0.97318 | 0.97412 | 0.97280 | 0.97456 | 0.97607 |
| 110.0 | 0.96656 | 0.97251 | 0.96651 | 0.97171 | 0.97290 | 0.97057 | 0.97263 | 0.97359 | 0.97223 | 0.97404 | 0.97558 |
| 111.0 | 0.96588 | 0.97196 | 0.96583 | 0.97114 | 0.97236 | 0.96998 | 0.97207 | 0.97306 | 0.97167 | 0.97352 | 0.97509 |
| 112.0 | 0.96520 | 0.97140 | 0.96516 | 0.97058 | 0.97181 | 0.96939 | 0.97152 | 0.97253 | 0.97111 | 0.97300 | 0.97460 |
| 113.0 | 0.96452 | 0.97085 | 0.96448 | 0.97001 | 0.97127 | 0.96880 | 0.97096 | 0.97199 | 0.97055 | 0.97248 | 0.97411 |
| 114.0 | 0.96384 | 0.97029 | 0.96381 | 0.96944 | 0.97073 | 0.96821 | 0.97040 | 0.97146 | 0.96998 | 0.97196 | 0.97362 |
| 115.0 | 0.96315 | 0.96974 | 0.96313 | 0.96887 | 0.97018 | 0.96763 | 0.96985 | 0.97093 | 0.96942 | 0.97144 | 0.97313 |
| 116.0 | 0.96247 | 0.96918 | 0.96245 | 0.96830 | 0.96964 | 0.96704 | 0.96929 | 0.97040 | 0.96886 | 0.97092 | 0.97264 |
| 117.0 | 0.96178 | 0.96863 | 0.96178 | 0.96773 | 0.96909 | 0.96645 | 0.96873 | 0.96987 | 0.96830 | 0.97040 | 0.97215 |
| 118.0 | 0.96110 | 0.96807 | 0.96110 | 0.96716 | 0.96855 | 0.96586 | 0.96818 | 0.96933 | 0.96773 | 0.96988 | 0.97166 |
| 119.0 | 0.96041 | 0.96752 | 0.96042 | 0.96659 | 0.96800 | 0.96527 | 0.96762 | 0.96880 | 0.96717 | 0.96936 | 0.97117 |
| 120.0 | 0.95973 | 0.96696 | 0.95974 | 0.96602 | 0.96746 | 0.96468 | 0.96706 | 0.96827 | 0.96660 | 0.96884 | 0.97068 |
| 121.0 | 0.95904 | 0.96641 | 0.95906 | 0.96546 | 0.96691 | 0.96409 | 0.96650 | 0.96774 | 0.96604 | 0.96832 | 0.97019 |
| 122.0 | 0.95836 | 0.96585 | 0.95839 | 0.96489 | 0.96637 | 0.96350 | 0.96594 | 0.96720 | 0.96548 | 0.96780 | 0.96970 |
| 123.0 | 0.95767 | 0.96529 | 0.95771 | 0.96432 | 0.96582 | 0.96292 | 0.96538 | 0.96667 | 0.96491 | 0.96728 | 0.96921 |
| 124.0 | 0.95698 | 0.96474 | 0.95703 | 0.96375 | 0.96528 | 0.96233 | 0.96483 | 0.96614 | 0.96435 | 0.96676 | 0.96872 |
| 125.0 | 0.95629 | 0.96418 | 0.95635 | 0.96318 | 0.96473 | 0.96174 | 0.96427 | 0.96560 | 0.96378 | 0.96624 | 0.96823 |
| 126.0 | 0.95560 | 0.96362 | 0.95567 | 0.96261 | 0.96418 | 0.96115 | 0.96371 | 0.96507 | 0.96321 | 0.96572 | 0.96773 |
| 127.0 | 0.95492 | 0.96307 | 0.95499 | 0.96205 | 0.96364 | 0.96056 | 0.96315 | 0.96453 | 0.96265 | 0.96520 | 0.96724 |
| 128.0 | 0.95423 | 0.96251 | 0.95431 | 0.96148 | 0.96309 | 0.95997 | 0.96258 | 0.96308 | 0.96208 | 0.96468 | 0.96675 |
| 129.0 | 0.95354 | 0.96195 | 0.95363 | 0.96091 | 0.96255 | 0.95938 | 0.96202 | 0.96347 | 0.96152 | 0.96416 | 0.96626 |
| 130.0 | 0.95284 | 0.96140 | 0.95295 | 0.96034 | 0.96200 | 0.95880 | 0.96146 | 0.96293 | 0.96095 | 0.96364 | 0.96577 |
| 131.0 | 0.95215 | 0.96084 | 0.95227 | 0.95977 | 0.96146 | 0.95821 | 0.96090 | 0.96240 | 0.96038 | 0.96312 | 0.96528 |
| 132.0 | 0.95146 | 0.96028 | 0.95159 | 0.95921 | 0.96091 | 0.95762 | 0.96034 | 0.96186 | 0.95982 | 0.96260 | 0.96479 |
| 133.0 | 0.95077 | 0.95972 | 0.95091 | 0.95864 | 0.96036 | 0.95703 | 0.95978 | 0.96133 | 0.95925 | 0.96208 | 0.96430 |
| 134.0 | 0.95008 | 0.95917 | 0.95023 | 0.95807 | 0.95982 | 0.95644 | 0.95921 | 0.96079 | 0.95868 | 0.96156 | 0.96381 |
| 135.0 | 0.94939 | 0.95861 | 0.94955 | 0.95750 | 0.95927 | 0.95585 | 0.95865 | 0.96026 | 0.95812 | 0.96104 | 0.96332 |
| 136.0 | 0.94869 | 0.95805 | 0.94887 | 0.95694 | 0.95872 | 0.95526 | 0.95809 | 0.95972 | 0.95755 | 0.96052 | 0.96283 |

TABLE 4 Continued

| Temperature °F | Volume Correction to 60°F | | | | | | | | | | |
|-------------------|---------------------------|---------|-------------|--------------|---------|---------|-------------------------------------|----------|----------|---|---|
| | Benzene | Cumene | Cyclohexane | Ethylbenzene | Styrene | Toluene | m-Xylene and Mixed Xylenes | o-Xylene | p-Xylene | 300 to 350° Aromatic Hydrocarbons | 350 to 400° Aromatic Hydrocarbons |
| 137.0 | 0.94800 | 0.95749 | 0.94819 | 0.95637 | 0.95818 | 0.95468 | 0.95752 | 0.95919 | 0.98698 | 0.96000 | 0.96234 |
| 138.0 | 0.94730 | 0.95693 | 0.94751 | 0.95580 | 0.95763 | 0.95409 | 0.95696 | 0.95865 | 0.95641 | 0.95948 | 0.96184 |
| 139.0 | 0.94661 | 0.95637 | 0.94683 | 0.95524 | 0.95708 | 0.95350 | 0.95640 | 0.95811 | 0.95584 | 0.95896 | 0.96135 |
| 140.0 | 0.94591 | 0.95581 | 0.94614 | 0.95467 | 0.95654 | 0.95291 | 0.95583 | 0.95758 | 0.95528 | 0.95844 | 0.96086 |
| 141.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95471 | ... | ... |
| 142.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95414 | ... | ... |
| 143.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95357 | ... | ... |
| 144.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95300 | ... | ... |
| 145.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95243 | ... | ... |
| 146.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95186 | ... | ... |
| 147.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95129 | ... | ... |
| 148.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95072 | ... | ... |
| 149.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.95015 | ... | ... |
| 150.0 | ... | ... | ... | ... | ... | ... | ... | ... | 0.94958 | ... | ... |

6.2 *Converting Volume to Weight for Mixtures—Chemicals Listed in Table 1—Correct* Convert the measured bulk volume to gallons at 60°F as described in 6.1. Determine the density (all weights *in vacuo*) at 60°F in grams per millilitre (or milliliter (equivalent to grams per cubic centimetre, they are equivalent) centimeter and kilograms per liter) as described in Section 7. To obtain the density in weight multiply the density in pound per gallon and the volume in gallons. To obtain the density in pounds per gallon *in vacuo*, *vacuo* multiply by the factor described in footnote C of multiple the measured density by 8.345404452. Table 1. To obtain the density in pounds per gallon *in air* at 60°F, use the equation described in footnote D of following equation to determine the pound per Table 1 gallon (or *in air*, refer to Appendix X3).

$$D_{\text{lb per gallon in air at 60 F}} = [1.000149926 \times D_{\text{in vacuo at 60 F}} - 0.00119940779543] \times 8.345404452$$

To obtain the weight in pounds, multiply the density in pounds per gallon by the volume in gallons.

6.2.1 *Example 3—If* The density of the *p*-xylene in Example 2 is less than 100% pure, its density should be determined by actual measurement. For1 was determined by Test Method D4052 instance, if the *p*-xylene is 95% pure and its density has been measured and determined to be 0.8651 to be 0.8646 g/mL (*in vacuo*) at 60°F, the density in lb/gal is: 60°F. The weight is:

$$\begin{aligned} & (0.8651 \times 8.34540438) \\ & = 7.2196 \text{ lb/gal in vacuo} \end{aligned}$$

$$\begin{aligned} & 9280 \text{ gal} \times 0.984143256178277 \times 8.345404452 \times 0.8646 \\ & = 65.897.4967627663 \text{ lb}_{\text{in vacuo}} \end{aligned}$$

or

$$\begin{aligned} & (0.8651 \times 1.00014992597 - 0.00119940779543) \times 8.34540438 = 7.2107 \\ & \text{lb/gal in air} \end{aligned}$$

$$\begin{aligned} & 9280 \text{ gal} \times 0.984143256178277 \times 8.345404452 \\ & \times [1.000149926 \times 0.8646 - 0.0011994077951] \\ & = 65.815.960860521 \text{ lb}_{\text{in air}} \end{aligned}$$