



**SLOVENSKI STANDARD**  
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**Nanotehnologije - Analiza nanoobjektov s frakcioniranjem asimetričnega in centrifugalnega pretoka skozi polje (ISO 21362:2026)**

Nanotechnologies - Analysis of nano-objects using asymmetrical flow and centrifugal field-flow fractionation (ISO 21362:2026)

Nanotechnologien - Analyse von Nanoobjekten mit Hilfe von Asymmetrischer-Fluss-Feldflussfraktionierung und zentrifugaler Feldflussfraktionierung (ISO 21362:2026)

Nanotechnologies - Analyse des nano-objets par fractionnement flux asymétrique et flux force centrifuge (ISO 21362:2026)

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Nanotehnologije

Nanotechnologies

**SIST EN ISO 21362:2026**

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## Nanotechnologies - Analysis of nano-objects using asymmetrical flow and centrifugal field-flow fractionation (ISO 21362:2026)

Nanotechnologies - Analyse des nano-objets par  
fractionnement flux asymétrique et flux force  
centrifuge (ISO 21362:2026)

Nanotechnologien - Analyse von Nanoobjekten mit  
Hilfe von Asymmetrischer-Fluss-  
Feldflussfraktionierung und zentrifugaler  
Feldflussfraktionierung (ISO 21362:2026)

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Ref. No. EN ISO 21362:2026 E

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## European foreword

This document (EN ISO 21362:2026) has been prepared by Technical Committee ISO/TC 229 "Nanotechnologies" in collaboration with Technical Committee CEN/TC 352 "Nanotechnologies" the secretariat of which is held by AFNOR.

This European Standard shall be given the status of a national standard, either by publication of an identical text or by endorsement, at the latest by August 2026, and conflicting national standards shall be withdrawn at the latest by August 2026.

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**International  
Standard**

**ISO 21362**

**Nanotechnologies — Analysis of  
nano-objects using asymmetrical  
flow and centrifugal field-flow  
fractionation**

*Nanotechnologies — Analyse des nano-objets par fractionnement  
flux asymétrique et flux force centrifuge*

**First edition  
2026-02**

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CH-1214 Vernier, Geneva  
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### Foreword

ISO (the International Organization for Standardization) is a worldwide federation of national standards bodies (ISO member bodies). The work of preparing International Standards is normally carried out through ISO technical committees. Each member body interested in a subject for which a technical committee has been established has the right to be represented on that committee. International organizations, governmental and non-governmental, in liaison with ISO, also take part in the work. ISO collaborates closely with the International Electrotechnical Commission (IEC) on all matters of electrotechnical standardization.

The procedures used to develop this document and those intended for its further maintenance are described in the ISO/IEC Directives, Part 1. In particular, the different approval criteria needed for the different types of ISO documents should be noted. This document was drafted in accordance with the editorial rules of the ISO/IEC Directives, Part 2 (see [www.iso.org/directives](http://www.iso.org/directives)).

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This document was prepared jointly by Technical Committee ISO/TC 229, *Nanotechnologies* and Technical Committee IEC/TC 113, *Nanotechnology for electrotechnical products and systems*, in collaboration with the European Committee for Standardization (CEN) Technical Committee CEN/TC 352, *Nanotechnologies*, in accordance with the Agreement on technical cooperation between ISO and CEN (Vienna Agreement). The draft was circulated for voting to the national bodies of both ISO and IEC.

This first edition cancels and replaces ISO/TS 21362:2018, which has been technically revised.

The main changes are as follows:

- addition of [subclause 8.6](#) addressing alternative and emerging methods;
- revision of technical content to reflect the current state of the art;
- addition of [Annex A](#) summarizing an interlaboratory comparison conducted through VAMAS.

Any feedback or questions on this document should be directed to the user's national standards body. A complete listing of these bodies can be found at [www.iso.org/members.html](http://www.iso.org/members.html).

## ISO 21362:2026(en)

### Introduction

The capacity to isolate and analyse diverse populations of nano-objects and their agglomerates or aggregates, often suspended in, or extracted from, complex matrices, is critical for applications ranging from materials discovery and nanomanufacturing to regulatory oversight and environmental risk assessment. Furthermore, the ability to characterize these analytes with minimal perturbation of their natural or native state is highly desirable. The list of available techniques capable of achieving such objectives is relatively short, and while all techniques have advantages and disadvantages, and no single technique is solely adequate or appropriate for all possible applications and materials, a group of related separation techniques known collectively as field-flow fractionation (FFF), conceptually proposed in Reference [1] offers many advantages for nanotechnology applications. In FFF, the analyte, suspended in a liquid medium, is fractionated by the application of a field (e.g. flow, centrifugal, electric, thermal-gradient, magnetic) perpendicular to the direction of flow of the analyte and mobile phase eluting through a thin defined channel. Separation occurs when the analyte responds to the applied field, such that populations with different response sensitivities reach equilibrium positions (i.e. in equilibrium with diffusional forces) higher or lower in the laminar flow streamlines perpendicular to channel flow, thus eluting differentially.

Among the FFF variants, asymmetrical flow FFF (variously abbreviated in the literature as AF4, A4F, AFFFF, AfFFF or AsFIFFFF) and centrifugal FFF (abbreviated as CF3, also called sedimentation FFF associated with the abbreviation SdFFF), are available commercially and have been most widely adopted in the nanotechnology field (for convenience and simplicity, the abbreviations AF4 and CF3 are used throughout this document). AF4 is arguably the most versatile technique with respect to the wide range of applications, materials and particle sizes to which it has been applied. Symmetrical flow FFF (fFFF), the original “flow-based” technique as first described in 1976,[2] has been supplanted commercially by AF4, introduced in 1987,[3] due to several advantages, including a simpler channel design, the ability to visualize the sample through a transparent top channel wall, and reduced analyte band width. The theory and application of CF3 as it is presently applied was described in 1974,[4] although a centrifugal field-based FFF system was first developed and tested independently in 1967.[5] Other FFF field variants, such as thermal, electrical and magnetic, provide unique capabilities, but are limited in the scope of their applications vis-à-vis nanotechnology or commercial availability.

Where FFF was once predominantly the domain of specialists, these instruments are now commonly and increasingly utilized in government, industry and academic laboratories as part of the nano-characterization toolbox. Two factors are driving this increase in nanotechnology utilization: maturation of commercial instrumentation and versatility with respect to coupling a wide range of detectors to FFF systems. In the latter case, recent developments have led to the use of highly sensitive elemental detectors (e.g. inductively coupled plasma mass spectrometer or ICP-MS), which offer enhanced characterization and quantification for many materials. Additionally, traditional concentration or sizing detectors, such as ultraviolet-visible (UV-Vis) absorbance, fluorescence, multi-angle light scattering (MALS) and dynamic light scattering (DLS), yield online data for eluting populations, and theoretically provide more accurate information than obtainable using off-line measurements of unfractionated polydisperse systems. The measured retention time of an eluting peak can also be used to estimate the hydrodynamic size by AF4 based on theoretical relationships or calibration with a known size standard. CF3 has the unique capacity to rapidly separate species of the same size but differing in density.

Although FFF based techniques have the capacity to separate and characterize analytes over an extremely broad size range, from about 1 nm up to tens of micrometres, this document focuses primarily on materials in the nanoscale regime and their associative structures. However, the basic underlying principles, experimental approach, and hardware described here can be more broadly applied.

For general references and further reading for FFF theory and practise, as well as AF4 and CF3 applications to nanotechnology, see References [6] to [18]. [Annex A](#) summarizes a Versailles Project on Advanced Materials and Standards (VAMAS) interlaboratory comparison conducted to evaluate the capacity of AF4 and CF3 techniques to separate and characterize components of a complex multimodal mixture of analytes reproducibly and with acceptable recovery and resolution across laboratories using different commercial instrument platforms and instrument configurations.

# Nanotechnologies — Analysis of nano-objects using asymmetrical flow and centrifugal field-flow fractionation

## 1 Scope

This document describes the general principles of field-flow fractionation and specifies parameters, conditions and minimal reporting requirements, as part of an integrated measurement system, required to develop and validate methods for the application of asymmetrical flow and centrifugal field-flow fractionation in the analysis of nano-objects and their aggregates and agglomerates in aqueous media. General guidelines and procedures are provided to aid the user.

## 2 Normative references

The following documents are referred to in the text in such a way that some or all of their content constitutes requirements of this document. For dated references, only the edition cited applies. For undated references, the latest edition of the referenced document (including any amendments) applies.

ISO 80004-1:2023, *Nanotechnologies – Vocabulary — Part 1: Core vocabulary*

ISO/TS 80004-6:2021, *Nanotechnologies — Vocabulary — Part 6: Nano-object characterization*

## 3 Terms and definitions

For the purposes of this document, the terms and definitions given in ISO 80004-1 and ISO/TS 80004-6 and the following, apply.

ISO and IEC maintain terminological databases for use in standardization at the following addresses:

- IEC Electropedia: available at <https://www.electropedia.org/>
- ISO Online browsing platform: available at <https://www.iso.org/obp>

### 3.1 nanoscale

length range approximately from 1 nm to 100 nm

[SOURCE: ISO 80004-1:2023, 3.1.1]

### 3.2 nano-object

discrete piece of material with one, two, or three external dimensions in the *nanoscale* (3.1)

[SOURCE: ISO 80004-1:2023, 3.1.5]

### 3.3 nanoparticle

*nano-object* (3.2) with all external dimensions in the *nanoscale* (3.1)

Note 1 to entry: If the dimensions differ significantly (typically by more than three times), terms such as nanofibre or nanoplate are preferred to the term nanoparticle.

[SOURCE: ISO 80004-1:2023, 3.3.4]

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### 3.4 field-flow fractionation FFF

separation technique where a field is applied to a liquid suspension passing along a narrow *channel* (3.7) in order to induce separation of the particles present in the liquid, dependent on their differing mobility under the force exerted by the field

Note 1 to entry: The field can be, for example, gravitational, centrifugal, liquid flow, electrical or magnetic.

Note 2 to entry: Using a suitable detector after or during separation allows determination of the mean size and size distribution of *nano-object* (3.2) populations.

### 3.5 asymmetrical flow field-flow fractionation AF4

separation technique that uses a *cross flow* (3.19) field applied perpendicular to the *channel flow* (3.21) to achieve separation based on analyte diffusion coefficient or size

Note 1 to entry: Cross flow occurs by means of a semipermeable (accumulation) wall in the channel, while cross flow is zero at an opposing nonpermeable (depletion) wall.

Note 2 to entry: By comparison, in symmetrical flow, the cross flow enters through a permeable wall (frit) and exits through an opposing semipermeable wall and is generated separately from the channel flow.

Note 3 to entry: *Nano-objects* (3.2) generally fractionate by the “normal” mode, where diffusion dominates and the smallest species elute first. In the micrometre size range, the “steric-lift hyperlayer” mode of fractionation is generally dominant, with the largest species eluting first. The transition from normal to *steric-lift hyperlayer mode* (3.33) can be affected by material properties or measurement parameters, and therefore is not definitively identified; however, the transition can be defined explicitly for a given experimental set of conditions; typically, the transition occurs over a particle size range from about 0,5 µm to 2 µm.

Note 4 to entry: Including both normal and steric-lift hyperlayer modes, the technique has the capacity to separate particles ranging in size from approximately 1 nm to about 50 µm.

### 3.6 centrifugal field-flow fractionation CF3

separation technique that uses a centrifugal field applied perpendicular to a circular *channel* (3.7) that spins around its axis to achieve size separation of particles from roughly 10 nm to roughly 50 µm.

Note 1 to entry: Separation is governed by a combination of size and effective particle density.

Note 2 to entry: Applicable size range is dependent on and limited by the effective particle density.

### 3.7 channel

<field-flow fractionation> thin ribbon-like chamber with a parabolic flow profile required for separation under the influence of a field applied perpendicular to the *channel flow* (3.21)

Note 1 to entry: *Channel thickness* (3.9) can vary and is nominally determined by a *spacer* (3.8) insert, while fixed-height channels have a predefined thickness and do not use inserts.

Note 2 to entry: In *asymmetrical flow field-flow fractionation* (3.5), a trapezoidal channel is commonly used, typically with a maximum breadth of ca. 20 mm to 25 mm and length of ca. 100 mm to 300 mm.

Note 3 to entry: In *asymmetrical flow*, one channel surface [*depletion wall* (3.12)] is solid (impermeable) and the opposing surface [*accumulation wall* (3.11)] consists of a semipermeable membrane on a porous frit.

Note 4 to entry: In *centrifugal field-flow fractionation* (3.6), both the inner and outer walls of the channel are solid (non-porous) and the channel is curved. A trapezoidal channel is commonly used, typically with a breadth of 10 mm to 20 mm and length of 300 mm to 550 mm.

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### 3.8

#### spacer

<field-flow fractionation> thin plastic film with a cut-out that defines the thickness and lateral dimensions of the *channel* (3.7)

Note 1 to entry: Trapezoidal or rectangular cut-outs are most commonly used in *asymmetrical flow field-flow fractionation* (3.5).

Note 2 to entry: Typical spacer thickness used for separation of *nano-objects* (3.2) ranges from 190 µm to 500 µm.

Note 3 to entry: Fixed-height channels do not use a spacer; in this case the channel shape and thickness are predefined.

### 3.9

#### channel thickness

$w$

<field-flow fractionation> nominal thickness as defined by the *spacer* (3.8) or predefined in a fixed-height *channel* (3.7)

### 3.10

#### effective channel thickness

$w_{\text{eff}}$

<field-flow fractionation> varying from the nominal value due to compressibility or swelling of the semipermeable membrane at the *accumulation wall* (3.11)

Note 1 to entry: The value of the effective thickness can differ from the nominal value for a given *spacer* (3.8) and may be determined using a well-defined analyte of known diffusivity under the test conditions.

Note 2 to entry: The measured effective channel thickness can depend on other factors, such as interactions between the analyte and the membrane and variability in spacer manufacturing.

### 3.11

#### accumulation wall

surface of a *field-flow fractionation* (3.4) channel toward which sample components are forced by the applied field acting perpendicular to the *channel flow* (3.21)

Note 1 to entry: In *asymmetrical flow field-flow fractionation* (3.5), the accumulation wall is flat and consists of a semipermeable membrane on a porous frit substrate.

Note 2 to entry: In centrifugal field-flow fractionation, the accumulation wall is impermeable and curved, and is located farther from the axis of rotation relative to the *depletion wall* (3.12). In the rare case that the particles have a lower density than the aqueous medium, the depletion and accumulation walls are reversed.

### 3.12

#### depletion wall

surface of a *field-flow fractionation* (3.4) channel opposite the *accumulation wall* (3.11), which is depleted in analyte due to the movement of analyte toward the accumulation wall in the applied field

Note 1 to entry: In asymmetrical flow field-flow fractionation, the depletion wall is flat and impermeable.

Note 2 to entry: In centrifugal field-flow fractionation (3.6), the depletion wall is impermeable and curved, and located closer to the axis of rotation relative to the accumulation wall. When the effective particle density is lower than the density of the medium, the depletion and accumulation walls are reversed.

### 3.13

#### mobile phase

#### carrier liquid

#### eluent

liquid phase used to achieve separation and transport of analytes

Note 1 to entry: The eluent or mobile phase can contain one or more salts, surfactants, and other chemical constituents that are required for optimized separation and *recovery* (3.35) of an analyte.